

Lignin utilization: A review of lignin depolymerization from various aspects

Chonlong Chio^a, Mohini Sain^b, Wensheng Qin^{a,*}

^a Department of Biology, Lakehead University, 955 Oliver Road, Thunder Bay, Ontario, Canada P7B 5E1

^b Centre for Biocomposites and Biomaterial Processing, Faculty of Forestry, University of Toronto, Toronto, Ontario, Canada M5S 3B3

ARTICLE INFO

Keywords:

Lignin
Depolymerization
Pyrolysis
Catalysis
Biodegradation
β-O-4 cleavage

ABSTRACT

Lignin is the most abundant aromatic polymer in nature. Due to its high amount of phenolic compounds storage, lignin is considered as an alternative source for various polymers and biomaterials production. Except for the native lignin in lignocellulose, a massive amount of technical lignin is being produced daily all over the world. However, the complex structure and low reactivity of lignin limit its further applications and currently, most of the lignin is burned for generating energy. Therefore, the depolymerization of lignin is considered one of the important challenges in lignin utilization. Methods for lignin depolymerization can be divided into thermochemical treatment, mechanical treatment, chemical catalysis, and biological treatment. Different methods for lignin depolymerization, their characteristics and products are extensively discussed in this review.

1. Introduction

Due to the massive consumption of fossil fuel and its limited storage, alternative energy and chemical sources are urgently needed. Thus, using natural plant resource, lignocellulose, to produce bioethanol and energy has become a hot topic in various areas. One of the major methods to produce bioethanol is converting the cellulose and hemicellulose in the lignocellulosic materials. However, a large amount of lignin could be left as a by-product after the bioethanol production due to its low reactivity and marketing value [1]. Furthermore, lignin is also considered as a by-product in the pulping industry. Thus, besides converting cellulose to valuable products, converting lignin to other value-added products also attract various research attention.

Lignin is the most abundant natural phenolic polymers in the world. In nature, lignin polymer usually forms ether or ester linkages with hemicellulose which is also associated with cellulose. Therefore, these nature polymers construct a complicated and valuable lignocellulose polymer (Fig. 1). Different sources of lignocellulose contain different ratios of these constructive polymers. In hardwood stem, the xylem

usually contains 40–55% of cellulose, 24–40% of hemicellulose and 18–25% of lignin, while the softwood stem contains 45–50% of cellulose, 25–35% of hemicellulose and 25–35% of lignin [2].

Lignin has a complicated cross-linking structure and contains several functional groups within the molecule, including aliphatic hydroxyl, phenolic hydroxyl and methoxyl groups. These functional groups affect the reactivity and chemical properties of lignin, especially the hydroxyl groups and aromatic structure are the most critical functional groups to determine the characteristics of the polymers [3,4]. The aliphatic hydroxyl group usually is the most abundant hydroxyl group in lignin polymer. However, the ratios of these hydroxyl groups in different sources of lignin could be various [1].

The three major precursors of the lignin polymer are p-coumaryl alcohol, coniferyl alcohol and sinapyl alcohol (Fig. 2). Lignin from different plants is constructed by various percentages of these precursors. For instance, the lignin from softwood mainly contains coniferyl alcohol, around 90–95%, while the lignin from hardwood usually contains coniferyl and sinapyl alcohols, around 25–50% and 50–75%, respectively, and the lignin from grass typically contains all three

List of abbreviation: HBT, 1-hydroxybenzotriazole; ABTS, 2, 2'-azinobis (3 - ethylbenzothiazoline - 6-sulphonic acid); 5CVA, 5-carboxyvanillic acid; DDVA, 5, 5'-dehydrodivanillate; ATP, Adenosine triphosphate; GS-HPV, α-glutathionyl-β-hydroxypropiovanillone; ALDHs, Aldehyde dehydrogenases; Al₂O₃, Aluminum oxide; HPV, β-hydroxypropiovanillone; CsOH, Cesium hydroxide; Ca(OH)₂, Calcium hydroxide; *C. echinulata*, *Cunninghamella echinulata*; DyP, Dye-decolorizing peroxidase; FeSO₄, Ferrous sulfate; FeS, Ferrous sulfide; GSH, Glutathione; HPLC, High performance liquid chromatography; HPVZ, HPV oxidase; HL, Hydrolysis lignin; KL, Kraft lignin; LiP, Lignin peroxidases; LiOH, Lithium hydroxide; Mn(NO₃)₂, Manganese nitrate; MnP, Manganese-dependent peroxidases; w.t.%, Mass fraction; MA, Muconic acid; NAD⁺, Nicotinamide adenine dinucleotide; OL, Organosolv lignin; PCB, Polychlorinated biphenyls; PHAs, Polyhydroxyalkanoates; KOH, Potassium hydroxide; PAHs, Polycyclic aromatic hydrocarbons; *P. putida*, *Pseudomonas putida*; p-TsOH, P-toluene sulphuric acid; *R. jostii*, *Rhodococcus jostii*; SiO₂, Silicon dioxide; NaHS, Sodium hydrosulphide; NaOH, Sodium hydroxide; THF, Tetrahydrofuran; TCA cycle, Tricarboxylic acid cycle; UV, Ultraviolet; *vdh*, Vanillin dehydrogenase; VA, Veratryl alcohol; VP, Versatile peroxidase

* Corresponding author.

E-mail address: wqin@lakeheadu.ca (W. Qin).

<https://doi.org/10.1016/j.rser.2019.03.008>

Received 10 December 2018; Received in revised form 24 February 2019; Accepted 4 March 2019

1364-0321/ © 2019 Elsevier Ltd. All rights reserved.

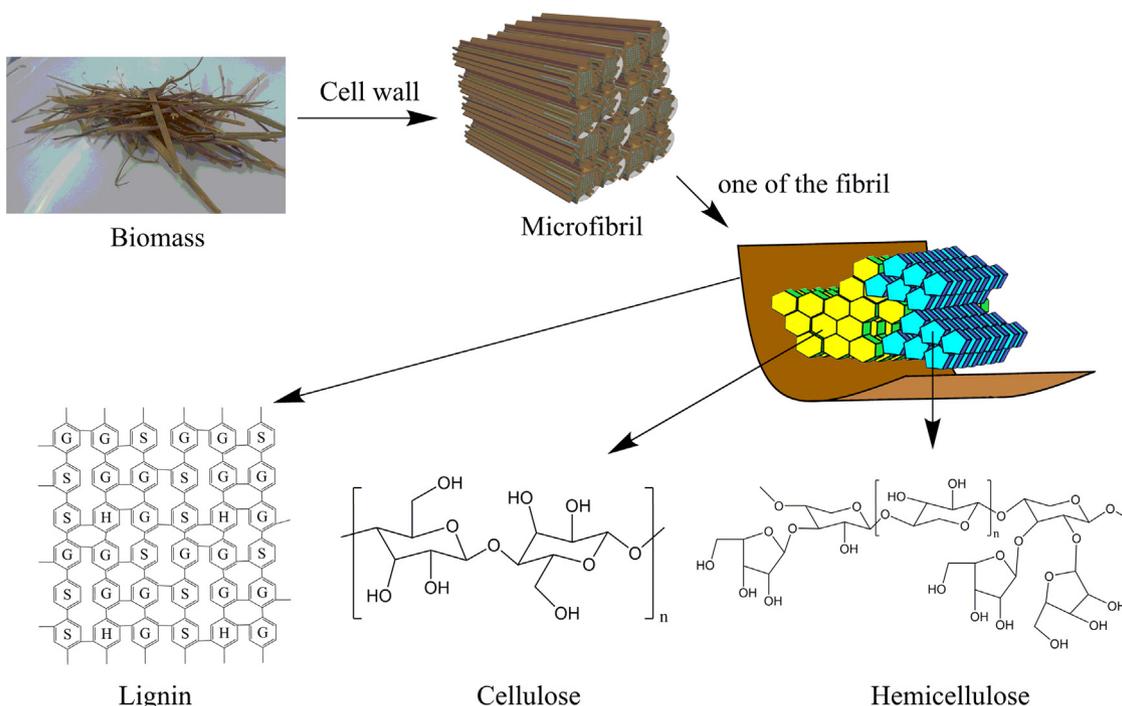


Fig. 1. Lignocellulose in biomass and its composition.

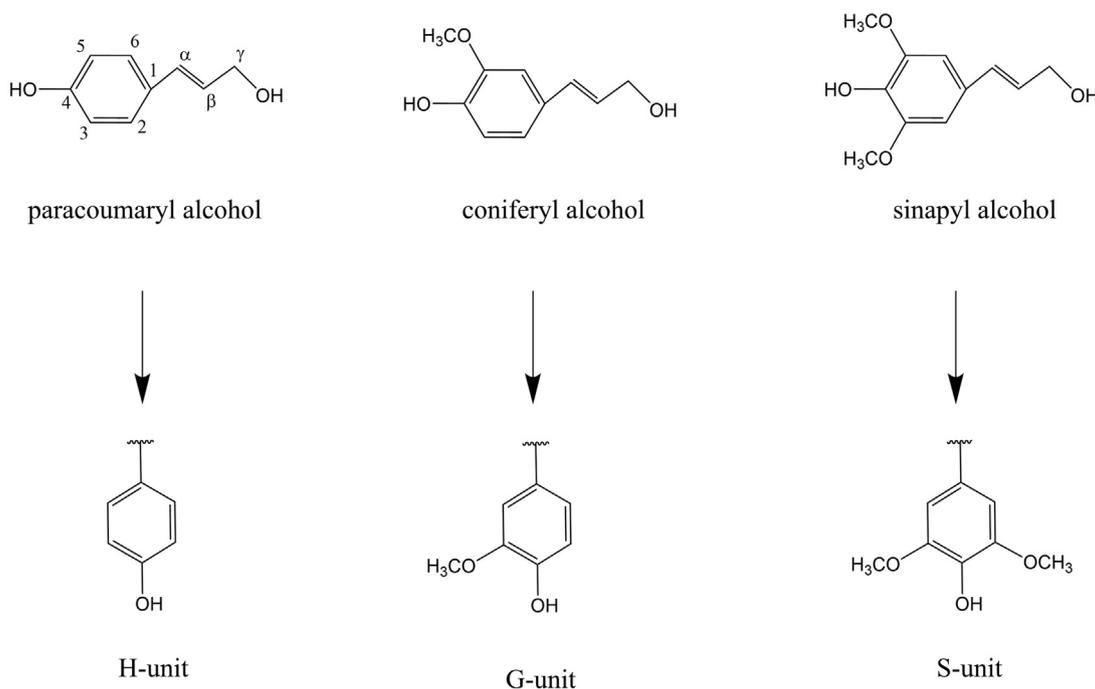


Fig. 2. The precursors and basic-unit in lignin molecule.

monomer alcohols [5,6]. There are two major linkages between these monomers: carbon-carbon linkages, also known as condensed linkages, and ether linkages (Fig. 3). The dominated linkage in the lignin polymer is ether linkages representing 56% or more in total linkages [7]. Due to the different ratios of these monomers in different sources of lignin, the exact ratios of linkages are also different in various species, like the most common ether linkages, β -aryl ether (β -O-4), represents around 50% and 60% of total linkages in softwood and hardwood, respectively [8]. Aryl ether linkage is easier to be cleaved when compared to condensed linkages during the lignin depolymerization and conversion [9],

thus the cleavage of the β -O-4 is also considered as a critical step of lignin depolymerization for utilizing lignin as raw materials to produce other chemicals [10]. In this review, we focus on introducing different aspects of depolymerization methods and using these techniques to produce lignin-derived materials.

Using technical lignin for different industrial applications has been studied for decades. The most common industrial application for kraft lignin is using it as fuel for heat generation. There are numerous studies investigating the potential application of lignin (Table 1) [11,12]. Furthermore, lignin also can be used as a sole carbon source for bacteria

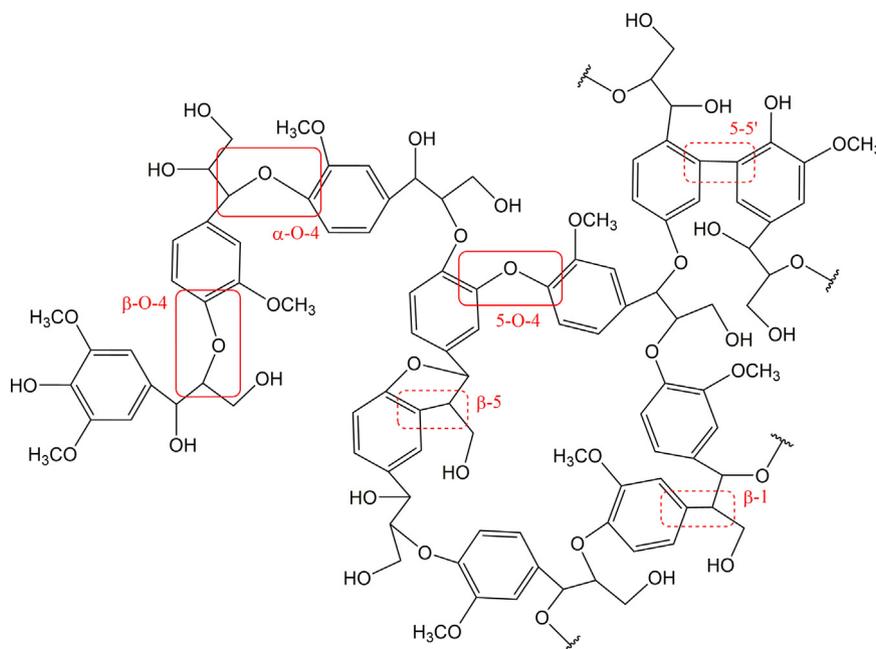


Fig. 3. Several typical linkages within the lignin molecule. The linkages marked by solid squares are ether linkages. The linkages marked by dot squares are condensed linkages.

culture [13] and produce triglyceride lipids during bacterial metabolism [14].

2. Lignin sources

Lignin can be classified as native lignin and technical lignin. Native lignin is referred to the original lignin structure in the lignocellulose without any modification. As a natural polymer, native lignin doesn't exist solely in nature. It always exists as part of the lignocellulose. Thus, most of the lignin being studied is modified lignin or technical lignin, which is the lignin extracted from biomass or recovered from the industrial by-product. Numerous studies are focusing on converting technical lignin to other value-add chemicals or products. The major source of technical lignin from industries is kraft lignin (KL) and there are several other types of lignin sources like hydrolysis lignin (HL), organosolv lignin (OL), pyrolytic lignin (PL), etc. The composition and molecular weight of these technical lignins are different according to their sources and extraction methods.

The technical lignin from the industrial by-product can be directly used as raw materials for other chemicals production. Aliphatic and aromatic hydroxyl groups are major constituents and active sites in technical lignin thus it also can be directly used as polyols for producing the polyurethane and replace 30% of petroleum-based polyols during the polyurethane production [21]. However, the reactivity of the technical lignin is much lower than the lignin fragment due to the reactive site is blocked by the complex structure. Compared to the

technical lignin, the depolymerized lignin fragment can replace up to 50% of the petroleum-based polyols during the polyurethane production [22]. Therefore, the depolymerization can enhance the availability of the lignin and expose more reactive sites which favor to further utilization [23].

2.1. Kraft lignin

The kraft process is one of the major traditional methods for pulping and paper production. It represents almost 80% of the chemical pulp production [24]. During the kraft process, the wood is treated with the solution of sodium hydroxide (NaOH) and sodium hydrosulphide (NaHS) under a temperature range of 150–170 °C. After several hours of treatment, the ether bonds in the lignin structure can be cleaved and converted to small lignin fragments which are also known as alkali-soluble lignin. Almost 90% of lignin of wood could become soluble during the delignification and the liquid mixture is named as black liquor [25]. Kraft lignin can be recovered by adding acid to acidify the black liquor to pH 5.0 or lower and it can be precipitated during the acidification. The advantage of using acidification to produce kraft lignin is that the Na^+ and S^{2-} in the solution mixture can be re-generated and reused in the kraft process [26,27]. This process has been already applied to the industrial production and introduced into the market. In 2013, 27, 000 t of kraft lignin were produced [28]. However, the current major application of the kraft lignin is used as fuel for energy production. The major reason for using it as fuel is related to its

Table 1

Potential application of lignin in various fields.

Applications	Descriptions
Energy production [15]	Lignin can be generated during the kraft process which also can be used as fuel for heat generation. Gasification of lignin also can produce syngas for energy production.
Dispersant [16]	Enhancing the dispersion of various insoluble particles like synthetic dye.
Biodegradable polymer [17]	Powdered lignin can be added during the polymer production and enhance the polymer biodegradability
Protective UV-absorbents [18]	Adding lignin to line fabrics can improve the UV barrier properties.
Nanoparticles [19]	By precipitating lignin in solution, a non-toxic and environmentally friendly nanoparticle can be produced. It can be further used in drug delivery and heavy metal absorption in the environment.
Phenolic resins [20]	Organosolv lignin can be directly replaced phenol which is used for phenol-formaldehyde resins production and it shows great curing properties compared to lignin free resins.

chemical properties. Kraft lignin is hydrophobic and it is not an active chemical compound unless it is modified to improve its reactivity. Kraft lignin also contains the aliphatic thiol groups which cause KL has a special odor [25,29].

2.2. Organosolv lignin

Lignin in the biomass can be dissolved in the organic solvent under certain condition and the lignin recovered from liquid fraction is named as organosolv lignin. Comparing to other lignin extraction methods, the organosolv process shows the ability to produce high-purity lignin from biomass, it also able to remain most of the cellulose residue for bioethanol production [30]. Therefore, the organosolv process is also considered as one of the promising methods for biomass utilization and organosolv lignin has become one of the famous technical lignin in the biorefinery. Previous studies have investigated various organic solvent including alcohol, acetic acid, ketone and ester [30–32] for dissolving different sources of lignin, including corn, wheat, pine wood, aspen trees and bamboo [33–37]. Organosolv lignin is also considered as one of the ideal lignin for biomaterial production due to its high purity, sulphuric-free and less modification which favor to the downstream process during the production [38].

2.3. Hydrolysis lignin

One of the promising applications of lignocellulose is ethanol production. Cellulose in the lignocellulose can be fermented to bioethanol with the help of various enzymes. However, the lignin in the lignocellulose forms a complex “shield” which blocks the interaction between enzyme and cellulose which lowers the yield of bioethanol production. The lignin which can't react with the enzyme is left as residue and become hydrolysis lignin [39]. The hydrolysis lignin contains 50–75% of lignin and other components like carbohydrate, mostly the untreated cellulose and oligosaccharides, nitrogen, etc. Comparing to kraft lignin, hydrolysis lignin is sulfur-free, has a low phenolic ratio and its structure is similar to the native lignin.

The potential applications of hydrolysis lignin include producing sorbents, resins, etc. [40,41]. Furthermore, the hydrolysis lignin has a higher reactivity than the kraft lignin due to its higher content of hydroxyl groups. It suggests that the hydrolysis lignin have a high potential for producing other polymeric chemicals [42,43]. However, its high impurity and low solubility restrict its applications [42]. Extensive studies had been focusing on using hydrolysis lignin but various studies indicated that the hydrolysis lignin needs multiple steps of modification and purification before applying to other usages [41], thus the major application of hydrolysis lignin is similar to kraft lignin, burnt as fuel and generating heat for energy production [44]. However, due to the numerous studies focus on using lignocellulose for biofuel production, using hydrolysis lignin for industrial applications can be a platform or direction in the future.

2.4. Pyrolytic lignin

Fast pyrolysis is one of the common methods for lignin conversion and depolymerization. After the pyrolysis, lignin or lignocellulose could be converted into a highly viscous bio-oil. A water-insoluble fraction can be obtained by adding water to the bio-oil and these water-insoluble solid are commonly known as pyrolytic lignin (PL). PL can be further purified by solubilizing in an organic solvent and removing the ash and other inorganic compounds. Unlike other technical lignin, PL is produced by the repolymerization of lignin oligomers during the pyrolysis. Various studies show that the polydispersity index of the switchgrass pyrolytic lignin (2.22–2.92) is significantly lower than the organosolv switchgrass lignin (4.3) which indicated that the pyrolytic lignin may be more uniform in particles mass [45,46].

There are various aspects of the potential applications of the

pyrolytic lignin. The study from Fortin et al. and Mullen et al. indicated that the non-purified pyrolytic lignin can provide more heating value during the combustion [46,47]. Except using for heat generation, pyrolytic lignin also can be used as raw material for value-added chemicals production. Gayubo et al. have proposed a strategy for separating pyrolytic lignin from cured bio-oil by co-feeding methanol. These processes are able to prevent the catalysts deactivation caused by the PL deposition and isolated the PL for further valorization [48]. Wang et al. supposed a cost-effective method for converting pyrolytic lignin to high purity value-added chemical hexamethylbenzene with the presence of the γ -Al₂O₃ under atmospheric pressure of N₂ [49]. Beside chemical production, pyrolytic lignin can be directly used as a starting material for producing carbon fiber with advance properties [50].

3. Thermochemical methods for lignin treatment

Increasing temperature is a common and effective treatment for destroying chemical bonds, thus the thermochemical and other physical treatments have attracted numerous researcher's attention. Thermochemical treatments include pyrolysis, hydrogenolysis, hydrolysis, etc. These treatments represent the thermal treatment of the lignin with or without other catalysts. The physical treatments are not only referring to mechanic treatment, but also include using other equipment-assistance for improving the depolymerization efficiency, like treatments with ultra-sonication and microwave, and these treatments usually have to involve other catalysts for completing the depolymerization.

3.1. Pyrolysis

Pyrolysis is one of the most widely studied methods for lignin or biomass depolymerization and conversion. Pyrolysis is a thermal treatment of organic substance without or under a limited amount of oxygen. Due to the absence of oxygen, the lignin is degraded but doesn't further convert to carbon dioxide. Most of the final products obtained from pyrolysis of lignin are liquids or gases. These products contain massive amounts of various aromatic monomer and they show a great potential that pyrolysis can be an effective method for converting lignin and biomass to other biomaterials [51]. In general, increasing the severity of the reaction condition can lower the molecular weight of the depolymerized lignin fragments [52]. Except for the severity of the reaction condition, the efficiency and the depolymerized products can be modified through several factors, including the source of lignin [53], solvent, catalysts [54], reaction time [55]. During the pyrolysis, lignin can be gasified and produce several gases at high temperature. These gases include hydrogen, carbon dioxide, carbon monoxide, and methane. The carbon monoxide and hydrogen mixed in the gases can be further processed to produce syngas for other applications [56,57].

Lignin depolymerization through pyrolysis usually starts with the cleavage of weak linkage at low temperature and further break down the strong linkages at higher than 450 °C. The depolymerized lignin fragments from the beginning stage are further converted to other chemicals at high temperature, including benzene ring cracking and gases release [58]. Pyrolysis can be performed in multiple ways but most of the pyrolysis process can be divided into two different stages: the first stage of pyrolysis and the secondary stage of pyrolysis [59].

The first stage of pyrolysis happens when the pyrolysis reaction temperature is within the range of 150–400 °C. Most of the ether linkages are destroyed including β -O-4 (Fig. 4) which is one of the most abundant linkages within the lignin molecule. The model chemical studies also indicated that the non-phenolic ether bonds are easier to be cleaved than the phenolic ether bonds and the condensed linkages like β -1 and biphenyl bonds also can be cleaved in this stage, even though it is not very effective [60]. Softwood lignin usually contains a greater number of condensed linkages than the hardwood lignin, thus softwood lignin usually lefts higher amount of residue than hardwood lignin

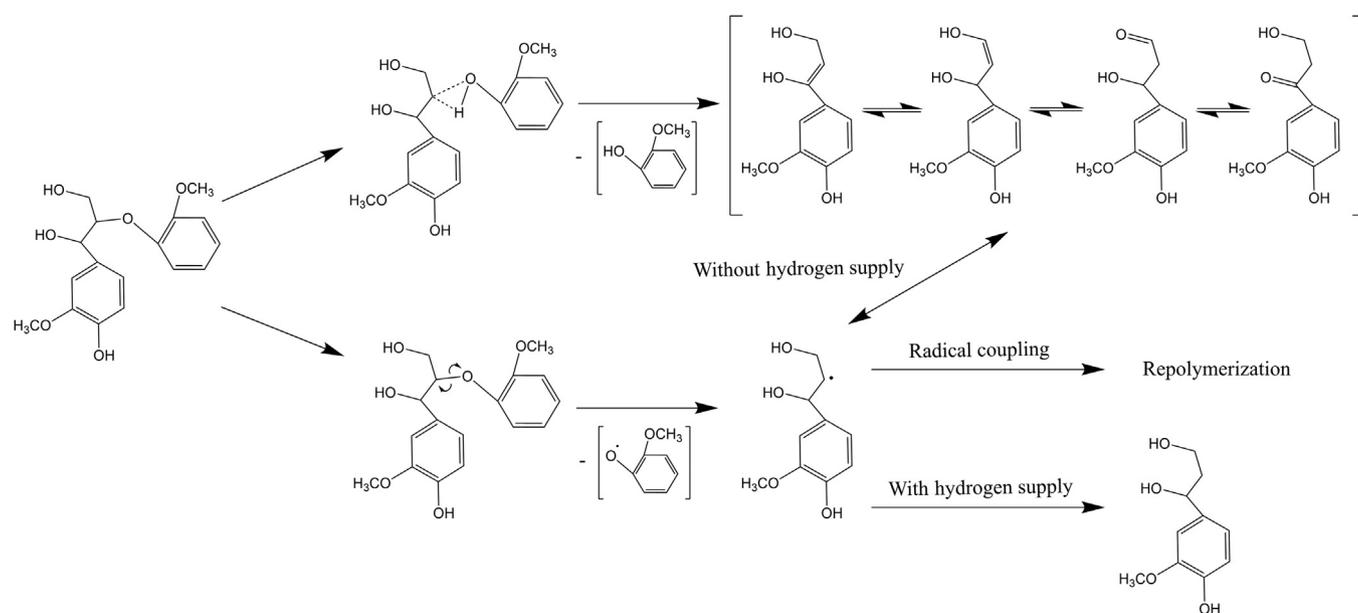


Fig. 4. The purpose mechanism of cleaving the β -O-4 linkages by pyrolysis.

[53]. During the first stage pyrolysis, the aromatic methylated groups and the condensed linkage are stable, therefore the depolymerized lignin fragments from first stage pyrolysis usually are the basic unit of lignin, like 4-methylguaiacol, syringol, coniferyl alcohol, and some lignin-derived chemicals like vanillin, isoeugenol or some unsaturated alkyl [61,62]. Under pyrolysis environment and without the hydrogen supply from the hydrogen donors, the amount of hydrogen is not enough for the depolymerized lignin fragments and other intermediates to form a stable chemical molecule, therefore these intermediates undergo the repolymerization and form the dimers or oligomers. Furthermore, the repolymerization process is trending to form the condensed bonds instead of ether bonds. Thus, the repolymerized products are more resistant to the depolymerization and increase the difficulty of further conversion. However, when the temperature reaches as 350 °C or higher, the hydrogen radicals released from lignin molecule can be sufficient for stabilizing the intermediates or depolymerized fragments, thus the yield of lignin-derived monomers could be increased [63–65].

The second stage of pyrolysis is the pyrolysis temperature higher than 400 °C and usually is up to 800 °C. Unlike the first stage pyrolysis, most of the linkages are broken down and the severer gasification starts during this stage. At 450 °C, the substituent methoxyl groups are cleaved and hydroxyl or methylated groups bonded to the aromatic units [66]. Therefore, the major products from first stage pyrolysis like syringols are further converted into *o*-vanillin, guaiacol and *o*-quinone methide [65]. When the pyrolysis temperature further increases to 550 °C, the benzene rings are broken down and converted into non-condensable gases [67]. The second stage pyrolysis product catechol can be degraded into carbon monoxide and cyclopentadienone which can be further decomposed into carbon monoxide and acetylene. Other products from second stage pyrolysis like pyrogallol can be converted to large amounts of carbon dioxide and carbon monoxide [68]. However, the formation of coke and polycyclic aromatic hydrocarbons (PAHs) lower the yields of the monomer and remain remarkable carbon content in the residue. The first stage of coke formation happens at 450 °C. Hosoya et al. indicated that the methoxyl group from guaiacol is responsible for the significant amount of coke formation [69]. The second stage of coke formation happened when the temperature is higher than 550 °C and various products are involved in the coke formation, including catechols, pyrogallols, and cresols. Previous studies also indicated that the increase of the methyl group in the depolymerized products could increase the yields of the coke formation [68]. Thus, the

methoxyl and methyl groups are one of the major reasons for the coke formation during the second pyrolysis. Moreover, due to the high percentage of methoxyl group presented in the syringol, syringol has a higher chance to form the coke during the pyrolysis and Asmadi et al. also shows that the yields of monomers from syringol are lower than the guaiacol [65]. However, Patwardhan et al. indicated that by increasing the pyrolysis temperature from 300 °C to 700 °C, 60% of the char formation could be suppressed and the yields of monomers including phenol, 2-methyl phenol, 2, 5- dimethyl phenol could be increased., especially with a high heating rate [3,55]. Windt et al. also suggested that low temperature and long reaction time increase the severity of the repolymerization [70]. Therefore, fast pyrolysis recently has attracted various attentions which can be considered as a better method for lignin thermochemical conversion.

Except for the usual pyrolysis, nowadays pyrolysis is commonly combined with various catalysts and solvents for improving its performance. Due to the closed environment during the pyrolysis, the addition of catalysts or solvents can offer several useful accompanying molecules like hydrogen donor or oxidant to improve the efficiency of pyrolysis by assisting demethoxylation or demethylation and providing sufficient hydrogen or hydroxyl group for preventing repolymerization and condensation. One of the well-known catalysts is zeolite. Most of the studies indicated that zeolite ZSM-5 with a wide range of Si/Al ratio can improve the efficiency of the depolymerization and increase the yields of aromatic monomers [61]. Furthermore, such zeolites can change the depolymerized lignin molecule dramatically by effectively converting lignin-derived phenolic compounds to aromatic hydrocarbons [71–73]. However, previous studies also indicated that the nature of pore on the zeolite causes the repolymerization and coke formation. Lignin which contains a high amount of simple phenols also causes the zeolites to deactivate quickly [61,74]. Some metal oxides also have been investigated as catalysts. Ma et al. show that cobalt can enhance the yields of various monomers and depends on the supporting materials like the ZSM-5 supported cobalt can convert lignin to aromatic hydrocarbons effectively. Furthermore, copper and nickel also can convert lignin to the specific phenolic product with high selectivity [75].

Pyrolysis can be an effective method for converting and liquefying lignin to bio-oil for other applications. However, the low-selectivity reaction limited its application in specific chemicals production. Furthermore, the severe reaction condition and short reaction time also

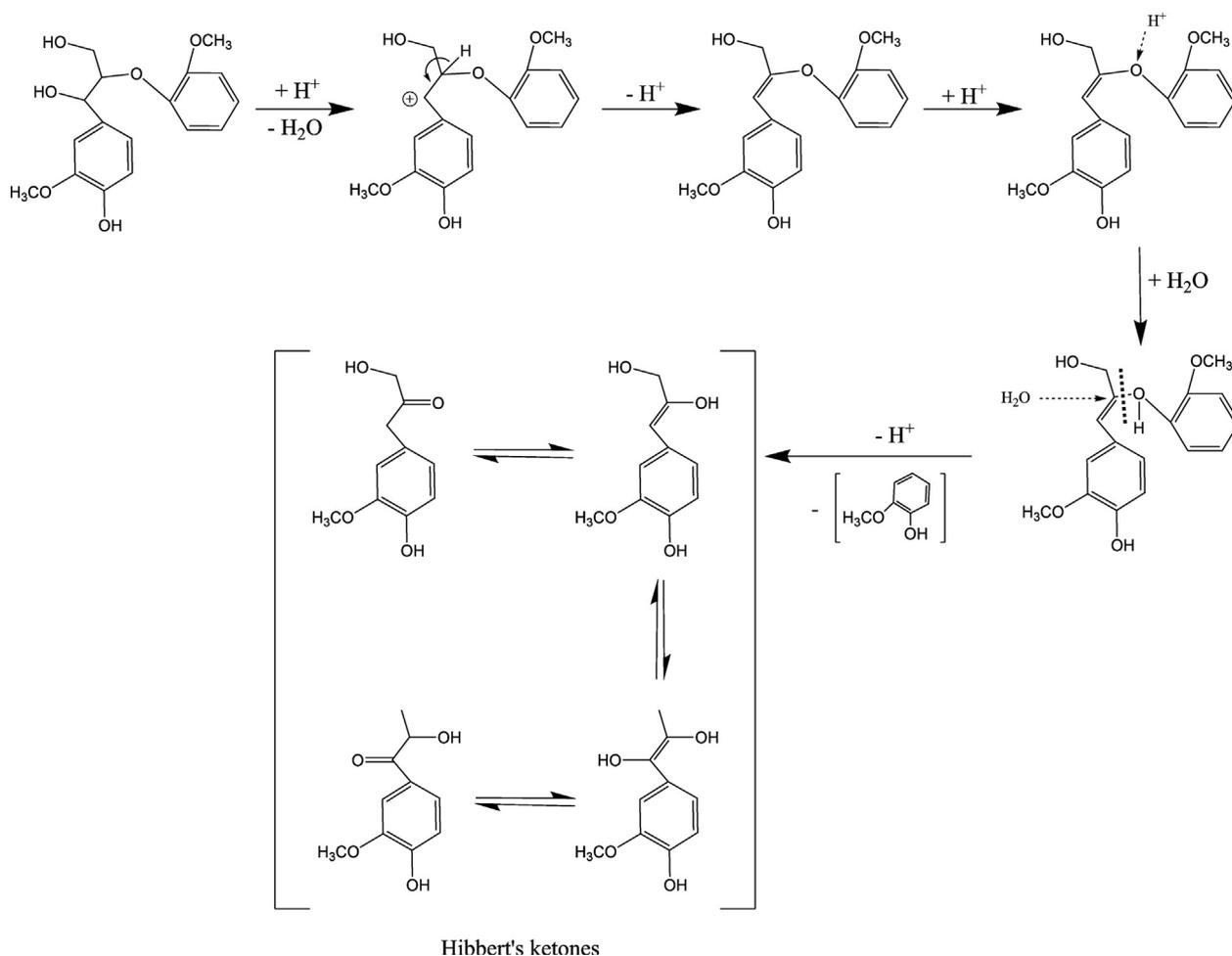


Fig. 5. The purpose mechanism of cleaving the β -O-4 linkages with acid-catalysts Adapted from [93].

cause the difficulty in product separation and restricted the studies on the mechanism of pyrolysis or catalyst-assisted pyrolysis which is favourable to valuable chemical production.

3.2. Microwave assisted depolymerization

The use of the microwave to assist the lignin or biomass conversion has been studied for decades [76,77]. Microwave can be an alternative method for heating instead of the traditional bath heating and it has been widely applied in the lignin and biomass thermochemical conversion [78]. Microwave can apply high energy of electromagnetic radiation into the lignin and biomass molecule. These radiations can cause the rotation of the polar molecules and ionic conduction, then further generating a massive amount of heat [79]. Therefore, compared with the traditional heating, microwave can prevent the physical contact between the heating source and material which can avoid the surface overheating and reduce the reaction time [77,80]. Moreover, the microwave is also proposed as an economic method for biomass heating and pyrolysis [81,82]. Liew et al. show that microwave pyrolysis could be an economic approach for converting biomass to valuable and high-quality active carbon [82] Furthermore, microwave contains lesser mechanic unit and can be accurately controlled during the operation [83].

Previous studies indicated that the use of microwave can improve the reaction selectivity with metal salt as catalyst. Zhu et al. use ferric sulfide as the catalyst and it further compares the performance of the microwave-assisted depolymerization to the traditional heating. The results indicated that the use of microwave can specifically cleave the

condense linkages $\text{C}\alpha\text{-C}\beta$ under 160 °C and it can enhance the ratio of soluble fraction from 67% to 86% [84].

Even though microwave is usually used as a heating method for lignin pretreatment or depolymerization with other catalysts, microwave also can be used as a heater for pyrolysis or pretreatment before pyrolysis. Using the microwave for pretreatment can cleave the weak linkage such as ether bond and remove the methoxyl group. Therefore, the char formation during the pyrolysis can be suppressed. Moreover, Duan et al. indicated that the microwave-assisted pyrolysis of alkali lignin can increase the yields of phenolic compounds like catechol, 2-methyl phenol from 3.81% to 14.15% and decreases the yields of guaiacols like creosol, eugenol from 36.56% to 22.36% at 200 °C, 60 min [85].

Except using for depolymerizing lignin, microwave also can be assisting liquefaction or solubilization of lignin by accelerating the heating rate. Due to the high heating rate, lignin can be easily dissolved in ionic liquid at a lower temperature and a shorter treatment period when compared to conventional heating methods [86]. During the heating, the electromagnetic field may also affect the chemical transformation and cause special thermal effects which are not able to be achieved by the traditional heating [87]. Furthermore, the biopolymers converted by microwave can be directly applied into the downstream process for polyurethane foam production [88,89] and these results show that the use of microwave for lignin liquefaction and biopolymers production has a great potential for industrial application.

4. Chemical or catalyst for lignin treatments

Based on the work of Wang et al., the chemical catalysts used for lignin depolymerization generally can be further divided into five different categories, including: (1) acid-catalyzed, (2) base-catalyzed, (3) metallic catalyzed, (4) ionic liquids-assisted catalyzed and (5) supercritical fluids-assisted catalyzed [90]. Except for the above categories, hydrogen peroxide also is one of the common catalysts for lignin depolymerization. Different chemical catalysts can be combined at the same time or applied into a different stage of the depolymerization process for improving the efficiency and producing desired products. These catalysts have their own advantages and disadvantages. Compared to the thermal treatment, the reaction condition is milder and the catalysis has a higher selectivity. However, environmental damages are also a major concern of using chemical catalysts.

4.1. Acid catalysts

Acid has been used as a catalyst for lignin depolymerization since 1943. The purposed mechanism of acid-catalysis of β -O-4 linkages is shown in Fig. 5. Hewson et al. indicate that combining ethanol and hydrochloric acid can depolymerize lignin and convert into several small molecules [91]. Except for using hydrochloric acid, other common acids also have been investigated. The diluted sulphuric acid also can carry out the depolymerization process while mixing with ethanol or water as a solvent [92]. The depolymerization process can be achieved under 2 MPa pressure and 250 °C for 1 h. The results show that using sulphuric acid as catalyst and 1:1 water-ethanol mixture as the solvent can produce 70 wt% depolymerized lignin. The depolymerized products are examined by H NMR and the result shows that the total hydroxyl number is around 442.0 mg KOH/g. Furthermore, around 87 wt% of carbon can be recovered from the lignin [24,92]. These results indicate that depolymerized lignin can be a suitable raw material for resins or foams production because these depolymerized products still remain a high amount of hydroxyl and carbon content.

Recently, p-toluene sulphuric acid (p-TsOH) is used as a hydrotrope to dissolve the lignocellulose in the purpose of delignification [94]. During the delignification, some of the depolymerized products can be produced. Even though the depolymerization is not effective, unlike other strong acid catalysts, it doesn't require harsh reaction condition. It can dissolve the lignin at 80 °C within 20 min. It provides a potential platform for low-cost acid-catalyzed depolymerization.

Even though the acid-catalyzed depolymerization is widely studied, there are several disadvantages which have to be overcome. It is widely reported that the depolymerization process requires relatively severe reaction condition like high temperature, high pressure, long reaction time and involve the use of corrosive chemicals. The wastes from the depolymerization process are also considered as environmental pollutants. Furthermore, repolymerization is always observed during the acid-catalyzed depolymerization [95]. The intermediates or depolymerized products could be condensed together and form macromolecules which could lower the yields of the desired products.

4.2. Base catalysts

Base catalyst also is a well-studied catalyst for lignin depolymerization. The purposed mechanism of base-catalysis of β -O-4 linkages is shown in Fig. 6. Thring et al. indicated that the use of sodium hydroxide can increase the yield of depolymerized lignin more than 4-folds when compared to the control which is without any alkaline [96]. Previous studies focused on using NaOH as the catalyst for lignin depolymerization due to the low cost and it was commonly used in industry. Yuan et al. indicated that with the presence of phenol, alkaline lignin can be almost completely degraded with 5% NaOH and only 1.4 wt% of solid is generated at 260 °C, 1 h [24,97]. Instead of using NaOH, multiple bases also have been studied, including KOH, CsOH, Ca(OH)₂, etc.

Interesting, Evans et al. indicated that using the strong bases, like KOH, NaOH, can convert and produce more depolymerized products rather than the weak bases, like Ca(OH)₂, LiOH [98]. Furthermore, the strong base also can reduce the char formation and remain the reactivity of the phenolic compounds during the depolymerization [99,100].

However, Knill et al. indicated that using a low concentration of base catalyst cannot catalyze the lignin depolymerization in water, almost no depolymerized products can be observed [102]. Therefore, most of the studies are using organic solvents, like ethanol, polyethylene glycerol, isopropanol, instead of water [92,103–105]. However, these organic solvents also can form a condensed structure with the lignin molecule [106]. Furthermore, the carboxylic acids which are produced during the depolymerization could further lower the pH of the reaction mixture and result in the repolymerization [107]. Thus, the repolymerization is also observed during the base-catalyzed depolymerization and this could lower the depolymerization efficiently and increase the amount of the residual lignin.

4.3. Metallic catalysts

Using acid or base catalyst is mainly focusing on the cleavage of the ether bonds. However, these methods are difficult to produce specific products. Furthermore, base or acid catalyzed depolymerization usually requires relatively severe reaction conditions, like high temperature (250 °C to higher than 300 °C) and high pressure (from 5 to 10 MPa) [108–110]. These conditions cause the depolymerization process to become costly and difficult to handle, thus numerous studies are looking for methods or catalysts which can catalyze the depolymerization process under a mild condition with high selectivity and several metals have been selected as potential catalysts for further study.

One of the most widely studied metallic catalysts is nickel. The purposed mechanism of metallic-catalysis of β -O-4 linkages is shown in Fig. 7. Song et al. indicated that metallic nickel can be a potential metallic catalyst to produce phenolic chemicals. Nickel is able to specifically cleave the ether linkages. Furthermore, it is able to hydrolyze the carbon-hydroxyl linkage at the side chain to alkane specifically [111]. Song et al. indicated that Ni can convert more than 50% of birch wood lignin to propylguaiacol and propylsyringol with high selectivity, 25% and 72% respectively, in ethyl glycerol at 200 °C, 6 h [112]. Furthermore, these studies also indicated that nickel can catalyze the depolymerization process under a mild reaction temperature (lower than 200 °C). Moreover, nickel combined with other metal can form bimetallic alloy Ni-M (M can be Ru, Rh, Pd, Au, Fe, Mo, Ti) [113–119]. Using bimetallic catalyst can increase the reactivity and selectivity due to the synergistic effect [120,121] and previous studies also indicated that these reactions can be achieved under 120 °C with high selectivity [113–115]. However, there are several limitations of the using nickel-bimetallic catalyst. The noble metals used in the bimetallic alloy are expensive which could increase the cost of the depolymerization. The noble metallic catalysts also cause the over-hydrogenation on the aromatic compounds under several reaction conditions which decreases the yield of the phenolic products. Thus, many efforts have been performed to lower the cost, including the use of cheap metal to replace the noble metal for synthesizing a non-precious alloy and improve these catalysts reusability [112,118,122].

Except for Ni, many metallic catalysts also have been studied including noble metals (Ru, Pd, Pt, Ti), cheap metals (Cu, Mo, Al, Fe, Zn), their combination and alloy [118,123–126]. Ye et al. show the potential of Ru in specifically converting corn stalk lignin to 4-ethylphenol and 4-ethylguaiacol with the yields of 3.10 wt% and 1.37 wt% at 275 °C, 90 min, 2 MPa [127].

Even though the metallic catalyst can catalysis and convert lignin to specific chemicals with high selectivity, the use of noble metal, catalyst deactivation and low conversion rate (around 50–60%) could limit the application of metallic catalysts in lignin depolymerization due to the cost of the processing, especially when compared to other chemicals

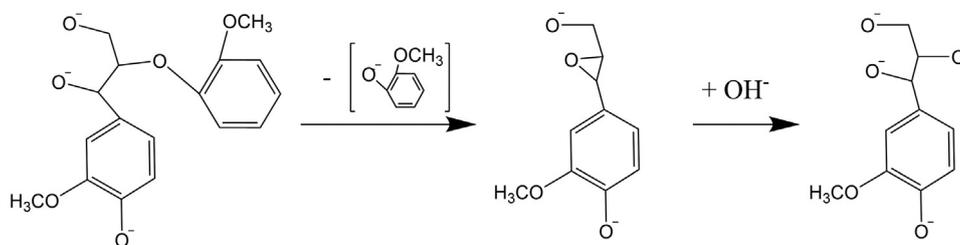


Fig. 6. The purpose mechanism of cleaving the β -O-4 linkages with base-catalysts Adapted from [101].

like acid, base which can almost completely convert lignin to other valuable chemicals during the reaction.

4.4. Ionic liquids assisted catalysis

The ionic liquid is widely defined as salts with a melting point less than 100 °C. Their unique physical and chemical properties have drawn remarkably attentions and these properties show the potential for industrial application including having a flexible characteristic which can be modified by changing the cation and anion in the salt, a low melting point and negligible vapor pressure which can convert salt to a high concentration ionic liquid easily and providing a strong environment for electrochemical reaction. Other properties like low volatility, inflammability, and high thermal stability also favor the industrial application [128].

The ionic liquid usually is used as a solvent and cooperates with other catalysts to depolymerize lignin due to that it is able to control the degree of the oxidation [129,130]. Several combinations of ionic liquid and metallic catalysts, including Cu, Mn, Co, have been studied. Stärk et al. reported that the combination of $\text{Mn}(\text{NO}_3)_2$ and 1-ethyl-3-methylimidazolium trifluoromethane sulfonate can selectively convert more than 63% of organosolv beech lignin to 2, 6-dimethoxy-1, 4-benzoquinone with the yield of 11.5 wt% at 100 °C, 24 h [131–133]. Interestingly, previous studies also indicated that the anion in the ionic liquid plays a critical role during the lignin depolymerization, thus it can significantly affect the yields of the monomeric products [132,134]. Furthermore, ionic liquid 1-octyl-3-methylimidazolium acetate has been studied as a catalyst for lignin depolymerization alone. It can convert more than 96% of lignin model molecules to phenolic compounds under mild reaction condition [130,135]. However, the high cost of the ionic liquid restricts its application and practice in the industrial operation. Furthermore, the ionic liquid usually has the interaction with the aromatic compound derived from lignin, thus it causes the difficulty of separating the ionic liquid from the monomeric products. This could become one of the major obstacles

for its application and the study from Dier et al. has tried to increase the reusability of the ionic liquid [136].

4.5. Sub- or supercritical fluids assisted catalysis

When solvents under extremely high temperature and pressure, they become sub- or supercritical fluids and exhibit several different properties when compared to ambient condition. Supercritical fluids usually contain both liquid and gas properties. They have low viscosity and high diffusivity which allow the fluids permeate into the lignin molecule structure. Furthermore, water under supercritical condition exhibit a low dielectric constant which is similar to a non-polar organic solvent, thus water can solubilize several organic compounds effectively [137]. Saisu et al. show that with the presence of phenol, almost all of the organosolv lignin can be depolymerized and converted into 2-cresol with the yield of 7.15 wt% by supercritical water at 400 °C, 1 h [138]. Similar researches had been conducted under different conditions, from 350 °C to 400 °C, and pressure, 25–40 MPa. The products from depolymerized lignin are further divided into methanol soluble and methanol insoluble. The soluble fraction mainly contains catechol, phenol and *o*, *m*, *p*-cresols. Previous studies also indicate that the repolymerization of low molecular weight molecule is observed in the supercritical condition [138–140]. Previous studies suggest that phenol can be added into lignin to inhibit the char formation and repolymerization [138,141,142]. The phenol can react with the decomposed fragment derived from lignin and block their active site for preventing the cross-linking reaction and repolymerization. The higher ratio of phenol to lignin shows a greater suppression [141,143]. However, the use of phenol for suppressing repolymerization is costly which would increase the expense in the overall process [144]. Except using supercritical water as the solvent, different supercritical organic solvents also have been applied in the depolymerization of lignin. Supercritical ethanol and methanol have been widely studied and performed in various conditions since the 1990s [98,145]. Cheng et al. reported that using supercritical ethanol for pine sawdust lignin depolymerization is more reactive and effective when compared to methanol. Only 12 wt% of

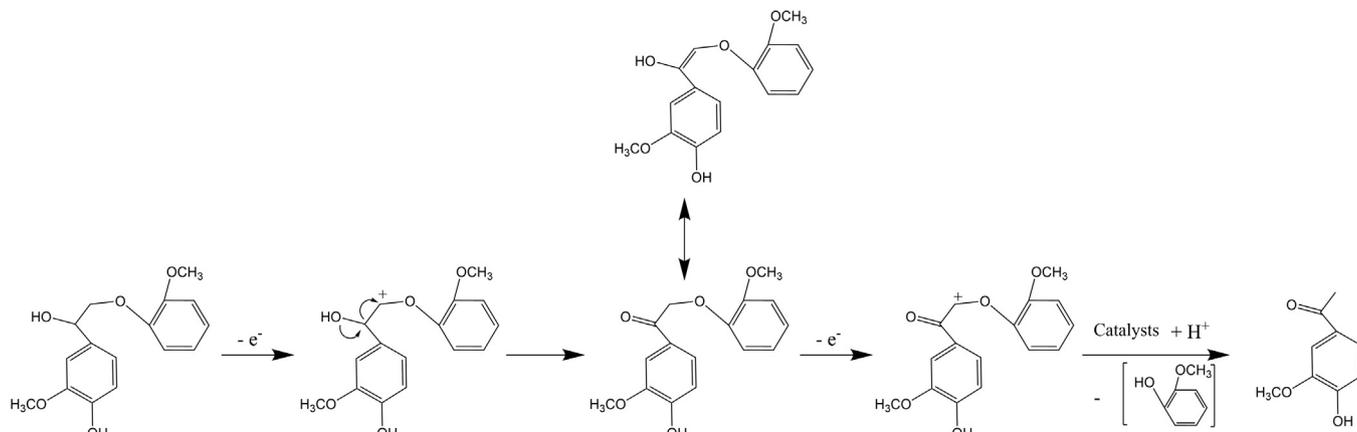


Fig. 7. The purpose mechanism of cleaving the β -O-4 linkages with the metallic catalyst.

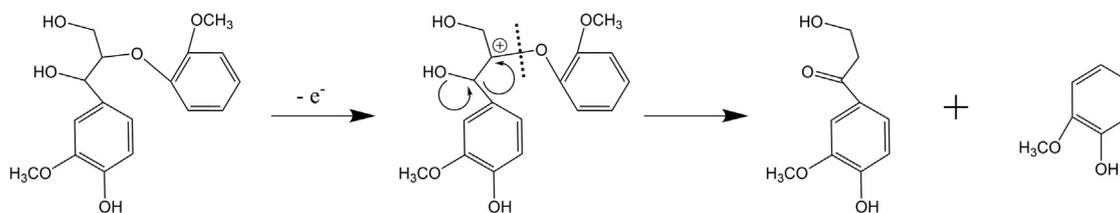


Fig. 8. The proposed mechanism of cleaving the β -O-4 linkages with the oxidant. The figure is showing one of the potential products. Actual products can be varied based on the oxidative degree.

solid is produced after the treatment at 300 °C, 20 min. Furthermore, 50% of ethanol or methanol can convert more than 95 wt% of pine sawdust lignin and produce 65 wt% of bio-oil which is 2-times higher than 100% ethanol or methanol [146].

Supercritical fluids can be an effective solvent for lignin depolymerization and solubilization. However, the high cost and severe reaction condition restricted its applications. Furthermore, the rapid hydrolysis of lignin in supercritical fluid enhance the difficulty of mechanism study and intermediate detection, thus the chemical conversion pathway need further study for improving selectivity and product separation.

4.6. Oxidative lignin depolymerization

Oxidation is one of the most common methods for lignin depolymerization and degradation [131,147,148]. The proposed mechanism of oxidation of β -O-4 linkages is shown in Fig. 8. Except for the chemicals in Sections 4.1 to 4.5, hydrogen peroxide and potassium permanganate are also widely used as oxidants for chemicals oxidation in industry or laboratory due to their high availability, low cost and easy to produce [148,149].

The use of hydrogen peroxide for lignin depolymerization or degradation has been well-studied for decades. Hydrogen peroxide usually combines with an appropriate catalyst like metallic catalysts or acid for selective lignin oxidation [150–152]. Hasegawa et al. used hydrogen peroxide to oxidize various type of lignin and their high performance liquid chromatography (HPLC) result shows that the alkali lignin can be depolymerized by 0.1% of diluted hydrogen peroxide and yield 45 wt% of formic, acetic acid and succinic acid at 200 °C, 5 min. Similarly, the diluted hydrogen peroxide can also convert the organosolv lignin to 20 wt% of these three organic acids [153]. Jennings et al. also indicated that hydrogen peroxide has the ability to oxidize β -O-4 and β -1 linkage specifically. They also show that lower the reaction time and temperature may enhance the reaction selectivity [151].

However, the hydrogen peroxide also causes the over-oxidation which lead the aromatic or phenolic compounds ring-opened and became alkylic compounds [154,155]. Furthermore, the over-oxidation turns the product become unspecific and difficult to control. This could increase the complexity of the mixture and difficulty of separating the products [151,156].

5. Biological depolymerization

Various chemical catalysts and thermochemical treatments have shown great potential for highly efficient lignin depolymerization. However, both of them require relatively severe reaction conditions, including high temperature and pressure. Furthermore, these processes usually have some environmental risk factors which may cause damages to the environment and require a massive amount of energy for operation [157]. Therefore, the use of biocatalysts has been considered as an alternative method for lignin depolymerization. Biocatalyst usually is considered as an environmentally friendly catalyst because the enzymes or microbes involved in the biological treatments usually are from nature and they are not harmful to the environment.

Furthermore, several enzymes can specifically catalyze the certain reaction, thus the use of biocatalyst can improve the reaction selectivity and suppress undesired side reaction such as repolymerization. Moreover, the biocatalyst required relatively milder reaction conditions when it compares to others, thus it lowers the requirement of the facility and reduces the formation of char. The biocatalysts use for lignin depolymerization and biomass treatment for various industrial applications like food, paper, and detergent have been studied for decades [158,159].

5.1. Organisms

Lignin is the most abundant phenolic polymer in nature and during a long time of evolution, numerous organisms have developed an effective metabolic system and methods to degrade and convert lignin to aromatic compounds and further convert these compounds to energy by multiple pathways [160].

5.1.1. Bacteria

Bacteria are considered as lesser effective than fungi in lignin degradation and one of the reasons is that there are fewer species in bacteria which are able to degrade lignin. However, several bacteria strains have been identified that it is suitable for lignin depolymerization and conversion. *Rhodococcus jostii* RHA1 is one of the well-studied lignin degraders and it has a great performance in consuming lignin to other compounds with the assistance of various enzyme [161]. Sainsbury et al. suggest that *R. jostii* RHA1 can cleave the β -O-4 with the help of dye-decolorizing peroxidase (DyP) and result in producing vanillin as the product [162]. Furthermore, Seto et al. also indicated that *R. jostii* RHA1 can degrade polychlorinated biphenyl and the further genomic studies also show that *R. jostii* RHA1 contains gene *benABCD* which can translate to various enzymes like 2-hydro-1,2-dihydroxybenzoate dehydrogenase for cleaving the linkage between biphenyl [163,164]. Therefore, *R. jostii* RHA1 also shows great potential for cleaving one of the common condensed linkage 5–5' within the lignin molecule. Moreover, Sainsbury et al. also knock out the vanillin dehydrogenase from *R. jostii* RHA1 and the mutated *R. jostii* RHA1 can accumulate a certain level of vanillin in the cell. Salvachua et al. also indicated that *R. jostii* RHA1 is a robust bacteria for genetic engineering because the mutated bacteria can grow under high cell density environment with limited nutrients and have the ability to tolerate toxic metabolites [165,166].

Except for *R. jostii* RHA1, *Pseudomonas putida* KT2440 is also known as an excellent lignin degrading bacterium [166]. Previous studies indicated that *P. putida* can be a good candidate for degrading lignin to low molecular-weight molecule, then produce and accumulate polyhydroxyalkanoates (PHAs), one of the potential raw materials for bioplastic production, by converting lignin-derived aromatic compounds from lignin-rich medium [166–168]. Further genetic studies are conducted including domestication and pathway engineering. Martinez-Garcia et al. have eliminated 300 genes in the *P. putida* KT2440 genome and the engineered strain have significant improvement in almost all of the physiological status, including reducing the lag-phase, increasing the biomass yields, growth rate and tolerance to oxidative stress

[169,170]. Further pathway studies indicated that mutated *P. putida* can accumulate PHAs as metabolic intermediates by using several aromatic compounds as raw materials. However, using lignin as the carbon source for *P. putida* culture has not been tested yet [171]. Except for PHAs, pyruvate and *cis, cis* muconic acid (MA), which have the great potential for various bioplastic production, are able to be converted from lignin-derived aromatic compounds by introducing additional enzymes. These products can be further accumulated in the cell by blocking the specific metabolic pathway [172,173].

Amycolatopsis sp. is widely studied due to its effective depolymerization ability and high conversion rate of high molecular weight lignin when it compares to other bacteria [166]. Due to the well-understanding of several aromatic metabolism pathways in *Amycolatopsis* sp. [174,175], several metabolic engineering studies have been completed recently. Similar to *R. jostii* RHA1, Fleige et al. identified and cloned the vanillin dehydrogenase (*vdh*) from *Amycolatopsis* sp. 39116 genome. After the verification, they successfully increased the yield of vanillin 2.3 times by knocking out the *vdh*. Due to the gene knock out, the bacterium is not able to use vanillin as sole carbon resource for energy production, thus vanillin produced from ferulic acid is accumulated in the cells (Fig. 9). However, the study also indicated that vanillin could enter an alternative pathway which could slowly oxidize vanillin to energy [176]. Except for vanillin, MA also is one of the valuable chemicals can be recovered from lignin depolymerization. Barton et al. used genetic engineered *Amycolatopsis* sp. 39116 to produce and accumulate MA from depolymerized lignin lysate. The gene *catB*, which is an essential enzyme for utilizing MA for further metabolism, is knocked out, thus the MA can't be further oxidized and accumulated in the cell. Even though the deletion affects the cell growth rate, the mutant can accumulate 3 times more MA than the wild-type [177].

Although various bacteria show their potential in lignin degradation and conversion, the conversion efficiency of bacteria is much lower than fungi, especially white- and brown-rot fungi. Ahmad et al. reported that the activities of the extracellular enzyme for lignin degradation in bacteria are significantly lower than the enzyme from fungi. Furthermore, Salvachúa et al. show that after 7 days incubation, *R. jostii* is only able to convert 20% of dark shaded bars lignin and 27% of it with the presence of glucose [166,178]. Moreover, genetic modification cannot be applied to all bacteria species due to the lack of related genetic information [179].

5.1.2. Fungi

The fungus is one of the most studied microbes for lignin

depolymerization and degradation. White rot basidiomycetes have been extensively studied in various aspects. They show a higher conversion rate and depolymerization efficiency when it compares to bacteria [166]. Due to strong ability in degrading lignin, white rot fungi have been applied into various industrial applications, including removing phenolic compounds from pollutants, delignification of biomass and increasing the cellulose ratio and improving biomethane production [180–184].

White rot fungi are the most effective microbe for degrading the native lignin in the wood [185]. Its great ability for degrading lignin may strongly relate to that white rot fungi can produce various extracellular oxidases including lignin manganese, laccases, and phenol oxidases [186]. The excessive amounts of these oxidases secretion also make the white rot fungi has an excellent performance in lignin degradation. *Phanerochaete chrysosporium* shows very high efficiency in removing lignin from biomass or waste, up to 99% [8,187]. Baltierra-Trejo et al. indicated that the strain *Pleurotus ostreatus* can effectively depolymerize lignin and produce several useful compounds like ferulic acid, syringyl alcohol [188]. Some fungi are able to depolymerize lignin and use the low molecular weight lignin or monomers as the carbon source for lipid synthesis. *Aspergillus fumigatus* is used for the fermentation of the wheat straw lignin-rich fraction and after the fermentation, various valuable chemicals are detected including syringic acid and vanillic acid, several short-chain fatty acids, including acetic acid and butyric acid are also detected [189]. However, Xie et al. cannot demonstrate that the fatty acid is mainly converted from lignin or another carbon source. A similar result has been presented by using a unique strain *Cunninghamella echinulata* FR3 which can effectively accumulate lipid by degrading lignocellulose. Moreover, Fenseca et al. also indicated that *C. echinulata* FR3 can degrade lignin with higher efficiency than cellulose or hemicellulose [190].

There are several genetic, proteomic and pathway studies focusing on improving the fungi performance and our understanding of how fungi depolymerize lignin. A laccase-encoding gene *lac I* has been isolated and identified from *Phlebia brevispora*. This gene is further cloned and transformed into *Pichia pastoris* for protein expression. The expression study indicated that *lac I* enzyme shows a high tolerance to various salt and solvents which shows its potential for using in various industrial applications [191]. Moreover, a novel laccase gene *lcc1* was isolated from *Ganoderma tsugae*. The knockout experiments show that *lcc 1* play an important role in lignin degradation. Furthermore, the depletion of *lcc 1* also has significant effects on the development of the mycelium and fruitbodies [192]. Proteomic studies indicated that

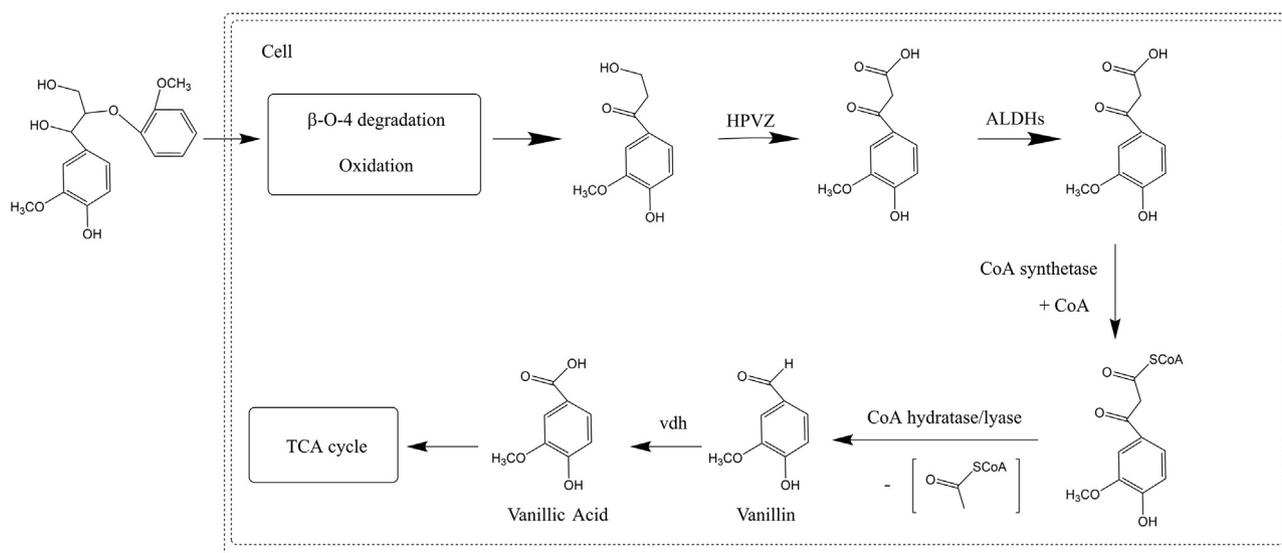


Fig. 9. The purpose pathway of converting lignin-derived compounds to energy.

manganese peroxidases and laccases are the most common lignin-degrading enzymes in basidiomycetes. Interestingly, several laccases show that they have the optimal reaction pH at 7 but usually these laccases also perform efficient and active in many different industrial environments [193]. Recently a novel β -etherase, which involved in the specific cleavage of β -O-4 linkage, is found in the *Dichomitus squalens*. Interestingly, a similar gene can be widely detected in various fungi or bacteria genomes but only a few of these species can exhibit the enzyme activity [194,195]. However, even though numerous genetic and pathway studies have been completed, unlike bacteria, a limited amount of studies are using metabolic engineering for improving valuable chemical production.

Extracellular laccase and various peroxidase are the major approaches for the fungi to degrade the lignin. However, even though fungi are more effective in lignin degradation when compared to bacteria due to the powerful extracellular enzyme, similar to other biological lignin depolymerization, the efficiency of the enzyme is much lower than chemical catalysis. Furthermore, the oxidoreductases produced by basidiomycetes also cause the lignin fragments repolymerization [196].

5.2. Enzymes

Enzymes which can effectively degrade lignin have been isolated from the fungi or bacteria and these enzymes have been applied in several *in vitro* experiments for lignin depolymerization or conversion study. Using *in vitro* enzymatic reaction can avoid several drawbacks including reducing the culturing time and the direct encounter between microbe and substrate [197]. Most of the *in vitro* experiments are conducted by using a single enzyme for cleaving lignin-model molecule as substrate. Other more complicated enzymatic digestion systems need a further understanding of molecular mechanism [198]. According to their reaction mechanism and environment, the enzyme for lignin degradation can be further classified as *in vitro* enzyme, mainly peroxidase and laccases, and *in vivo* enzyme.

5.2.1. *In vitro* enzymes

Most of the enzyme we found which can degrade lignin is non-specific cleavage. These enzymes mostly come from two enzyme families: peroxidase and laccase. Both of these enzymes catalyze the lignin by oxidation. Instead of catalyzing specific substrates or linkages, they attack the lignin molecule randomly. There are two groups of peroxidases have been well-studied, lignin peroxidases (LiP) and manganese-dependent peroxidases (MnP). Recently, versatile peroxidase (VP) and dye-decolorizing peroxidase (DyP) also attract various studied interest due to their versatile properties.

5.2.1.1. Laccases. Laccase is one of the common oxidases that can be isolated from various fungi and bacteria [199]. The most effective lignin-degrader white wood fungi also is one of the major laccase producers [193]. Laccase is a blue-copper phenoloxidase which can use oxygen as an electron acceptor and oxidize phenolic compounds (Fig. 10). The oxidized phenolic compounds could be converted into phenoxyl free radical which is an unstable intermediate and it could further lead to the polymer cleavage [200].

Even though the activity of laccase is limited to phenolic compounds, laccase also can cooperate with the mediator and degrade non-phenolic compounds [201]. The mediators are some small molecules which have the ability to transfer the electron, such as 2, 2'-azinobis (3-ethylbenzothiazoline - 6-sulphonic acid) (ABTS) and 1-hydroxybenzotriazole (HBT). These accompany molecules can assist laccase to form a stable intermediate with the substrate [202]. With the help of the mediator, laccase can degrade almost 80–90% of lignin structure [203]. Numerous studies tried to increase our understanding of the laccase at the genetic level and improve its performance and stability. Laccase also can be applied in several treatments except for

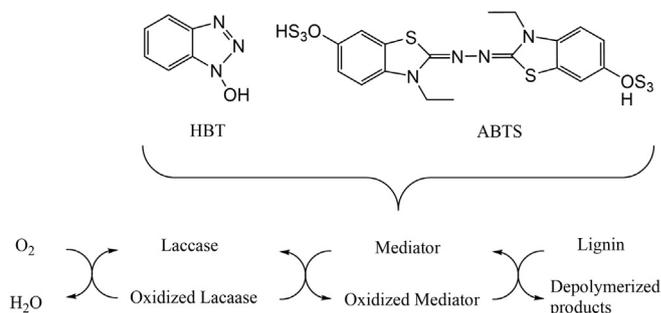


Fig. 10. The mechanism of laccase mediated lignin degradation.

depolymerization, including lignin-like chemical conversion, delignification [204–206]. Interesting, even though laccase plays an important role in lignin depolymerization, laccase is not an essential enzyme for microbes to depolymerize lignin. Previous studies indicated that even though with the limited amount or without the presence of laccase, the microbes are still able to degrade lignin [207,208].

5.2.1.2. Lignin peroxidases. Lignin peroxidase (LiP) also has been isolated from various fungi. LiP is a glycoprotein and it contains a heme group in its active center and it has a range of molecular weight from 38 to 43 kDa [186]. It requires hydrogen peroxide for initiating and catalyzing the non-phenolic compounds and phenolic compounds [209] (Fig. 11). It also required veratryl alcohol as an electron donor and cofactor to complete the catalytic cycle [210]. LiP also is known as the most effective peroxidase when compare to others peroxidases because it has a high redox potential which makes LiP able to oxidize various substrates which other peroxidases cannot oxidize [211]. Except using for lignin depolymerization, LiP is also used for delignification due to its great efficiency of removing lignin [212,213].

5.2.1.3. Manganese dependent peroxidases. Manganese dependent peroxidase (MnP) is an enzyme very similar to LiP. It is a glycosylated protein and needs hydrogen peroxide as an oxidant to initiate the catalytic cycle (Fig. 12). Afterward, MnP uses Mn^{2+} as reducing substrate and convert it into Mn^{3+} . The Mn^{3+} is a strong oxidant and it diffuses from the enzyme and starts to oxidize the lignin phenolic compounds. Therefore, the MnP can convert lignin phenolic compounds to phenoxy-radicals by Mn^{3+} and the phenoxy-radicals could cause the lignin depolymerization [214]. Similar to laccase, MnP plays an important role in the initial lignin depolymerization [215]. Furthermore, *in vitro* experiment indicated that the addition of MnP present in the system can enhance the effectiveness of the depolymerization process [216,217]. Usually, MnP only can oxidize phenolic compound, but MnP is also able to oxidize non-phenolic lignin model compounds with the presence of additional Mn^{2+} , previous studies also indicated that high level of Mn^{2+} can enhance the activity of MnP to degrade lignin in solid [218,219]. However, the repolymerization is also observed during the use of LiP and MnP for depolymerizing the synthetic lignin polymer [220,221].

5.2.1.4. Other peroxidases. Except for the enzymes mentioned in Sections 5.2.1.1 to 5.2.1.3, there are several peroxidases can be used for lignin depolymerization. Versatile peroxidase (VP) can be widely found in fungi *Bjerkandera* and *Pleurotus* and it has some similar catalytic properties with MnP and LiP [215,222]. VP is a bifunctionality enzyme. It can oxidize Mn^{2+} like MnP, it also able to oxidize various substrates which have high or low redox potentials like LiP [223,224]. However, unlike MnP, VP can oxidize Mn^{2+} independently [225]. The protein crystal structural studies also explain the bifunctionality of VP [225–227] and due to its bifunctionality, VP has attracted several research interests. Except using VP for lignin depolymerization, VP also can be used for

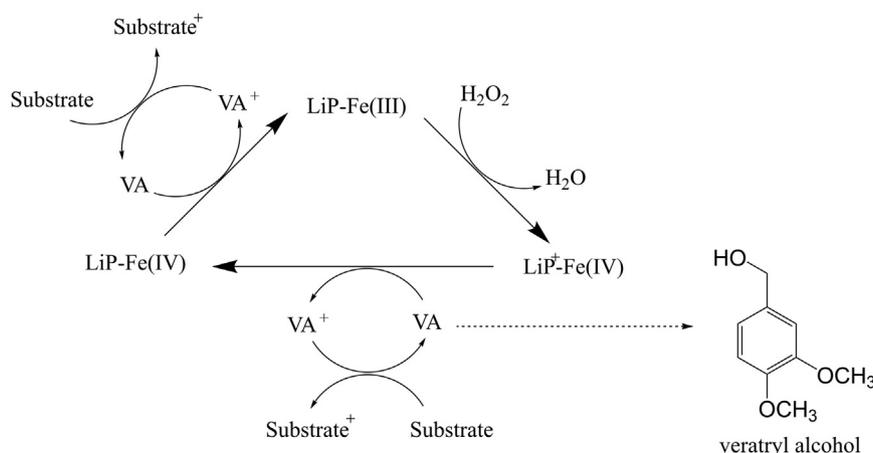


Fig. 11. The mechanism of LiP mediated lignin degradation.

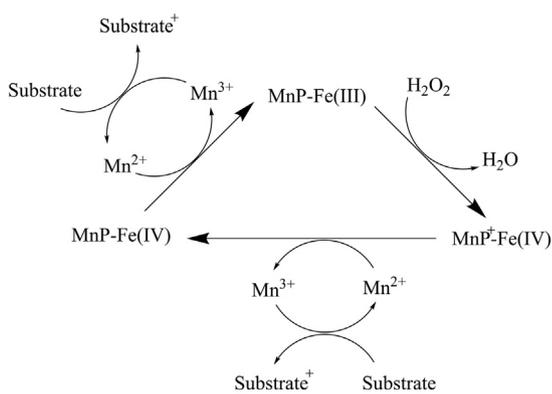


Fig. 12. The mechanism of MnP mediated lignin degradation.

delignification of biomass and decolorization of industrial waste [228,229]. The genetic studies related to VP also have been studied for a decade. The gene *mnp2* has been identified that it is responsible for encoding the VP and the inactivation of *mnp2* reduce the effectiveness of fungi in lignin degradation [230]. VP has been cloned and expressed in heterogeneous hosts, including *E. coli* and yeast, for the large-scale production and mutagenesis study [231–233].

Dye-decolorizing peroxidase (DyP) is another type of peroxidase which has been widely studied for lignin depolymerization. The first DyP was isolated from *Bjerkandera adusta* in 1999 [234]. The following studies also indicated that DyP unlike other peroxidases which are mainly found in fungi can be found widely in various bacteria [235,236]. Even though the sequence and structure of DyP are different from other peroxidases, they share similar catalytic properties and mechanism by using hydrogen peroxide and mediator for the substrate oxidation [237–239]. According to the sequence characteristics, DyPs can be classified into four classes [240]. Type A, B, and C can be widely found in the bacteria and type D are mostly produced by fungi [241]. Usually, type A and B DyP are produced by bacteria and they have a smaller size and lower activity. However, type C DyP is similar to type

D DyP, both of type C and D DyP have a higher activity for substrate oxidation [242]. These four classes of DyP both have peroxidase activity and characteristic. However, even though Mn²⁺ is a necessary mediator for type B DyP oxidation, some type A DyPs doesn't have the Mn²⁺ oxidation activity and it may oxidize substrates by other routes [243,244]. Interesting, there is a novel DyP has been recently identified and it can oxidize the substrate with the oxygen in the air and without the presence of hydrogen peroxidase [245]. The mutagenesis study also has been conducted in DyP from *Pseudomonas putida* MET94 to improve the DyP performance in the industrial application by direct evolution [246].

5.2.2. In vivo enzymes

Many peroxidases have been studied as *in vitro* enzyme because they oxidize the lignin molecule outside the organism. As mentioned in Section 5.2.1, these laccases and peroxidases attack the lignin randomly, then convert the phenolic group to free-radicals and these radicals lead to the lignin depolymerization. After the lignin has been degraded to small molecules, the bacteria take up these monomers or oligomers and these small molecules undergo a series of conversion catalyzed by various *in vivo* enzyme. Most of the linkages within the lignin molecules have their specific metabolic pathways to cleave these specific linkages. The understanding of the enzymes involved in the pathway can develop an efficient and reliable approach with high selectivity for lignin depolymerization and conversion.

5.2.2.1. β-O-4 ether degradation. The β-O-4 ether bond is one of the major linkages within the lignin molecule and it almost represents 50% or more of the total linkages. Therefore, cleavage of β-O-4 ether bond is considered as an important step for lignin depolymerization [247]. The cleavage of the β-O-4 ether bond has been studied in various organisms, including *Sphingobium* sp. SYK-6, *Novosphingobium* sp. PP1Y, *Novosphingobium aromaticivorans* and *Dichomitus squalens* [195,248–250]. Both of them have similar pathway and mechanism (Fig. 13). β-O-4 degradation starts with LigD, a α-dehydrogenase. LigD oxidizes the hydroxyl group at Cα position, then the β-etherase,

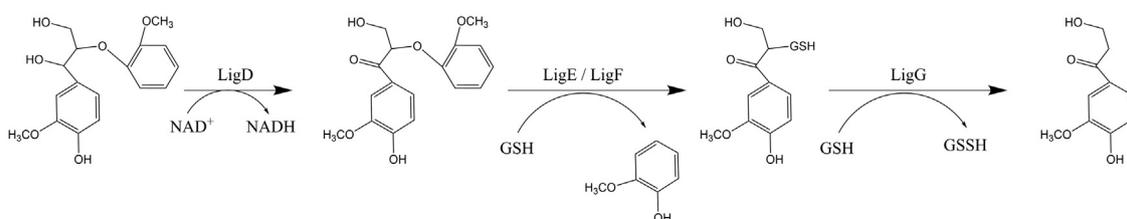


Fig. 13. The mechanism of LigDEF mediated lignin β-O-4 model molecule degradation.

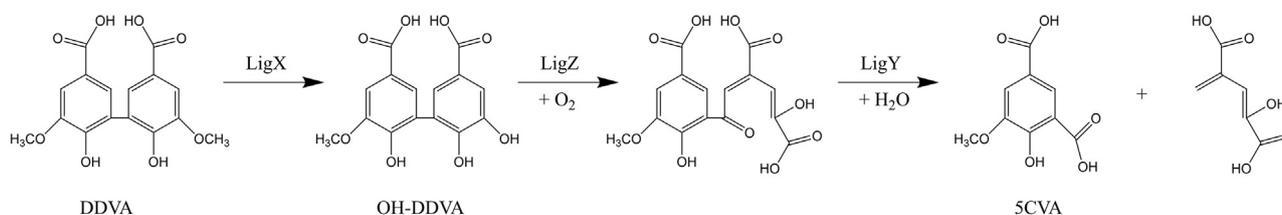


Fig. 14. The mechanism of LigXYZ mediated lignin 5–5' model molecule degradation.

Table 2

A brief summary of various lignin depolymerization methods.

	Methods	Advantages	Disadvantages
Thermochemical/Physical depolymerization	Pyrolysis	Rapid and easy to operate	Low selectivity in production, severe reaction condition and char formation
	Microwave-assisted	The operation can be precisely controlled and avoid surface heating	High energy consumption
Chemical catalysis	Acid-catalysis	Effective and low cost	Environmental concern and corrosive acid catalysts may cause repolymerization
	Base-catalysis		Costly and low conversion rate
	Metallic-catalysis	High selectivity	Difficult to separate the product from the mixture
	Ionic liquid-catalysis	Highly adjustable reaction	Severe reaction condition
	Supercritical fluid-catalysis	Effective	Over-oxidation and low selectivity
Biological depolymerization	Hydrogen peroxides catalysis	Low cost and facily produce	Low efficiency and long culture period
	Bacteria conversion	Eco-friendly and can be genetically engineered for specific chemical production	
	Fungal conversion	Eco-friendly and can be used for various technical lignin purification	
	<i>In vitro</i> enzyme depolymerization	Eco-friendly and able to produce specific chemical	
	<i>In vivo</i> enzyme depolymerization		

LigE or LigF, cleave the β -O-4 ether bond and generate vanillin and α -glutathionyl- β -hydroxypropiovanillone (GS-HPV) as intermediate. Finally, the GS-HPV is oxidized by LigG, glutathione-S-transferase. The glutathione is cleaved and the remaining β -hydroxypropiovanillone can be further oxidized to vanillin [247,251]. After the genes of LigD, E, F and G have been identified, several genetic pathway studies have been conducted. Interestingly, Sonoki et al. expresses the LigD, F, G in the plant *Arabidopsis thaliana* and the result shows that the gene LigD, F, G can introduce post-lignification modification by cleaving several β -ether linkages and enhance the enzymatic digestibility of the lignin produced by the plant [252].

5.2.2.2. Bi-phenyl degradation pathway. The biphenyl linkage represents 10% of the total linkages in softwood lignin [3]. The purposed mechanism of biphenyl linkages degradation is shown in Fig. 14. When the 5, 5'-dehydrodivanillate (DDVA) enters the organism, LigX, a DDVA O-demethylase, can demethylate one of the methoxy group and convert it to the hydroxyl group [253]. The product of LigX is the substrate for oxidative meta-cleavage by LigZ, OH-DDVA dioxygenase [254]. The product from LigZ is further hydrolyzed by LigY, a hydrolase for the meta-cleavage compound of OH-DDVA. Finally, after the cleavage of LigY, 4-carboxy-2-hydroxypentadienoic acid and 5-carboxyvanillic acid (5CVA) are generated and 5CVA is further converted into one of the metabolic central products vanillate [251]. The cleavage of bi-phenyl linkage have been widely studied due to this structure is highly similar to polychlorinated biphenyls (PCB), one of the major pollutants and carcinogens from industrial production [255].

Even though the *in vivo* enzymes show great selectivity when compare to peroxidases and laccases, most of their reactions require ATP and NADH as cofactors to complete the reaction, and these requirements restrict their performance in industrial applications [251]. Furthermore, the conversion rate is significantly lower than other methods.

6. Summary

In this review, we summarize a series of methods for lignin depolymerization and conversion. Different methods have their own advantages and limitations. The comparisons of various methods are provided in Table 2. It is difficult to simply rank the best lignin depolymerization method among these treatments because their characteristic and products are various. Therefore, understanding the characteristic of each depolymerization methods and applying the appropriate approach for the specific purpose is the best treatment for lignin utilization.

In the point of view of lignin valorization, pyrolysis is the most effective method for converting lignin and biomass to crude bio-oil for energy generation. Moreover, during or after the pyrolysis, several value-added products can be recovered which can be used for lowering the energy production cost. However, in the case of depolymerizing lignin for specific valuable chemical production, chemical catalysis should be considered as the most appropriate approach due to the high specificity and conversion rate. Furthermore, the reaction condition of the catalysis is milder than pyrolysis which decreases the difficulty of handling the facility and reaction. Biological depolymerization is also a promising method for lignin valorization. However, it is still not close to actual application in industry and there are many challenges have to be solved before applying the enzyme or bacteria in lignin valorization. The major problem is the low efficiency of converting lignin polymer to monomers or even other chemicals. However, the study in biological lignin depolymerization is still meaningful and valuable because these technologies also can improve our waste treatment in the phenolic polymer. Furthermore, phenol-degrading enzyme and enzymes like β -etherase which has the ability to cleave ether linkage specifically are rare in nature. Comprehensive studies on these related enzymes could provide us an alternative and environmentally-friendly approach in various chemical treatments.

It is no doubt that biomass and lignin can be a promising alternative resource for replacing petroleum. Various studies have demonstrated the valorization of lignin by directly modifying lignin for multiple

applications. Numerous studies also show the potential of using lignin depolymerization for valuable chemical production. However, most of these studies are focusing on lab scale of experiments. The characterization of the products from the upgraded scale of lignin depolymerization can advance the process of utilizing lignin depolymerization in chemicals production. Furthermore, various studies also propose strategies for establishing a cost-effective and convenient system for lignin utilization. These afford would become the foundation of biomass utilization and green future.

Acknowledgments

I would like to appreciate Dr. Jun Cui and Dr. Marianne Lee for their encouragement and support. Also, I would like to give my appreciation to my family, friends, and Hibiki for their supports.

Declarations of interest

None.

Funding

This work was supported by the Natural Sciences and Engineering Research Council Discovery Grant [grant numbers RGPIN-2017-05366] to WQ.

References

- [1] Li C, Zhao X, Wang A, Huber GW, Zhang T. Catalytic transformation of lignin for the production of chemicals and fuels. *Chem Rev* 2015;115:11559–624.
- [2] Howard R, Abotsi E, Van Rensburg EJ, Howard S. Lignocellulose biotechnology: issues of bioconversion and enzyme production. *Afr J Biotechnol* 2003;2:602–19.
- [3] Pandey MP, Kim CS. Lignin depolymerization and conversion: a review of thermochemical methods. *Chem Eng Technol* 2011;34:29–41.
- [4] Cateto CA, Barreiro MF, Rodrigues AE, Belgacem MN. Optimization study of lignin oxypropylation in view of the preparation of polyurethane rigid foams. *Ind Eng Chem Res* 2009;48:2583–9.
- [5] Dorrestijn E, Laarhoven LJJ, Arends IWCE, Mulder P. The occurrence and reactivity of phenoxyl linkages in lignin and low rank coal. *J Anal Appl Pyrol* 2000;54:153–92.
- [6] Zhongzheng L. Research on renewable biomass resource - lignin. *J Nanjing For Univ (Nat Sci Ed)* 2012;1:003.
- [7] Pu Y, Zhang D, Singh PM, Ragauskas AJ. The new forestry biofuels sector. *Biofuel Bioprod Biorefin* 2008;2:58–73.
- [8] Chen Z, Wan C. Biological valorization strategies for converting lignin into fuels and chemicals. *Renew Sustain Energy Rev* 2017;73:610–21.
- [9] Yuan Z, Cheng S, Leitch M, Xu CC. Hydrolytic degradation of alkaline lignin in hot-compressed water and ethanol. *Bioresour Technol* 2010;101:9308–13.
- [10] Reiter J, Strittmatter H, Wiemann LO, Schieder D, Sieber V. Enzymatic cleavage of lignin β -O-4 aryl ether bonds via net internal hydrogen transfer. *Green Chem* 2013;15:1373.
- [11] Thomas A, Pedram F. Production and application of lignosulfonates and sulfonated lignin. *ChemSusChem* 2017;10:1861–77.
- [12] Stewart D. Lignin as a base material for materials applications: chemistry, application and economics. *Ind Crops Prod* 2008;27:202–7.
- [13] Zhu D, Zhang P, Xie C, Zhang W, Sun J, Qian WJ, et al. Biodegradation of alkaline lignin by *Bacillus ligninophilus* L1. *Biotechnol Biofuels* 2017;10:44.
- [14] Bugg TD, Rahmanpour R. Enzymatic conversion of lignin into renewable chemicals. *Curr Opin Chem Biol* 2015;29:10–7.
- [15] Naqvi M, Yan J, Dahlquist E. Bio-refinery system in a pulp mill for methanol production with comparison of pressurized black liquor gasification and dry gasification using direct causticization. *Appl Energy* 2012;90:24–31.
- [16] Qin Y, Lin X, Lu Y, Wu S, Yang D, Qiu X, et al. Preparation of a low reducing effect sulfonated alkali lignin and application as dye dispersant. *Polymers* 2018;10:982.
- [17] Luo X, Xiao Y, Wu Q, Zeng J. Development of high-performance biodegradable rigid polyurethane foams using all bioresource-based polyols: lignin and soy oil-derived polyols. *Int J Biol Macromol* 2018;115:786–91.
- [18] Zimmiewska M, Kozłowski R, Batog J. Nanolignin modified linen fabric as a multifunctional product. *Mol Cryst Liq Cryst* 2008;484. [43/[409]–50/[16].
- [19] Frangville C, Rutkevicius M, Richter AP, Velev OD, Stoyanov SD, Paunov VN. Fabrication of environmentally biodegradable lignin nanoparticles. *Chemphyschem* 2012;13:4235–43.
- [20] Cetin NS, Özmen N. Use of organosolv lignin in phenol–formaldehyde resins for particleboard production: I. Organosolv lignin modified resins. *Int J Adhes Adhes* 2002;22:477–80.
- [21] Cateto CA, Barreiro MF, Rodrigues AE. Monitoring of lignin-based polyurethane synthesis by FTIR-ATR. *Ind Crops Prod* 2008;27:168–74.
- [22] Mahmood N, Yuan Z, Schmidt J, Xu CC. Depolymerization of lignins and their applications for the preparation of polyols and rigid polyurethane foams: a review. *Renew Sustain Energy Rev* 2016;60:317–29.
- [23] Arshanitsa A, Krumina L, Telysheva G, Dzhibite T. Exploring the application potential of incompletely soluble organosolv lignite as a macromonomer for polyurethane synthesis. *Ind Crops Prod* 2016;92:1–12.
- [24] Mahmood N, Yuan Z, Schmidt J, Charles Xu C. Production of polyols via direct hydrolysis of kraft lignin: effect of process parameters. *Bioresour Technol* 2013;139:13–20.
- [25] Doherty WOS, Mousaviou P, Fellows CM. Value-adding to cellulosic ethanol: lignin polymers. *Ind Crops Prod* 2011;33:259–76.
- [26] Olivares M, Guzman JA, Natho A, Saavedra A. Kraft lignin utilization in adhesives. *Wood Sci Technol* 1988;22:157–65.
- [27] Koljonen K, Österberg M, Kleen M, Fuhrmann A, Stenius P. Precipitation of lignin and extractives on kraft pulp: effect on surface chemistry, surface morphology and paper strength. *Cellulose* 2004;11:209–24.
- [28] Upton BM, Kasko AM. Strategies for the conversion of lignin to high-value polymeric materials: review and perspective. *Chem Rev* 2016;116:2275–306.
- [29] Lora JH, Glasser WG. Recent industrial applications of lignin: a sustainable alternative to nonrenewable materials. *J Polym Environ* 2002;10:39–48.
- [30] Kabir MM, Rajendran K, Taherzadeh MJ, Horváth IS. Experimental and economical evaluation of bioconversion of forest residues to biogas using organosolv pretreatment. *Bioresour Technol* 2015;178:201–8.
- [31] Wildschut J, Smit AT, Reith JH, Huijgen WJ. Ethanol-based organosolv fractionation of wheat straw for the production of lignin and enzymatically digestible cellulose. *Bioresour Technol* 2013;135:58–66.
- [32] Boeriu CG, Fițișău FI, Gosselink RJ, Frissen AE, Stoutjesdijk J, Peter F. Fractionation of five technical lignins by selective extraction in green solvents and characterisation of isolated fractions. *Ind Crops Prod* 2014;62:481–90.
- [33] Guo Y, Zhou J, Wen J, Sun G, Sun Y. Structural transformations of triploid of *Populus tomentosa* Carr. lignin during auto-catalyzed ethanol organosolv pretreatment. *Ind Crops Prod* 2015;76:522–9.
- [34] Huijgen W, Telysheva G, Arshanitsa A, Gosselink R, De Wild P. Characteristics of wheat straw lignins from ethanol-based organosolv treatment. *Ind Crops Prod* 2014;59:85–95.
- [35] Lv X, Li Q, Jiang Z, Wang Y, Li J, Hu C. Structure characterization and pyrolysis behavior of organosolv lignin isolated from corncob residue. *J Anal Appl Pyrolysis* 2018.
- [36] Zhang W, Tian G, Polle A, Janz D, Euring D, Yue X, et al. Comparative characterization of ethanol organosolv lignin polymer from bamboo green, timber and yellow. *Wood Sci Technol* 2018:1–11.
- [37] Domínguez J, Santos T, Rigual V, Oliet M, Alonso M, Rodríguez F. Thermal stability, degradation kinetics, and molecular weight of organosolv lignins from *Pinus radiata*. *Ind Crops Prod* 2018;111:889–98.
- [38] Asawaworarit P, Daorattanachai P, Laosiripojana W, Sakdaronnarong C, Shotipruk A, Laosiripojana N. Catalytic depolymerization of organosolv lignin from bagasse by carbonaceous solid acids derived from hydrothermal of lignocellulosic compounds. *Chem Eng J* 2019;356:461–71.
- [39] Dahlman O, Jacobs A, Liljenberg A, Olsson AI. Analysis of carbohydrates in wood and pulps employing enzymatic hydrolysis and subsequent capillary zone electrophoresis. *J Chromatogr A* 2000;891:157–74.
- [40] Yasuda S, Asano K. Preparation of strongly acidic cation-exchange resins from gymnosperm acid hydrolysis lignin. *J Wood Sci* 2000;46:477–9.
- [41] Rabinovich ML. Wood hydrolysis industry in the Soviet Union and Russia: a minireview. *Cell Chem Technol* 2010;44:173.
- [42] Liitia T, Rovio S, Talja R, Tamminen T, Rencoret J, Gutierrez A, et al. Structural characteristics of industrial lignins in respect to their valorization. 2014.
- [43] Nakagame S, Chandra RP, Kadla JF, Saddler JN. The isolation, characterization and effect of lignin isolated from steam pretreated Douglas-fir on the enzymatic hydrolysis of cellulose. *Bioresour Technol* 2011;102:4507–17.
- [44] Hamelinck CN, Hooijdonk Gv, Faaij APC. Ethanol from lignocellulosic biomass: techno-economic performance in short-, middle- and long-term. *Biomass-Bioenergy* 2005;28:384–410.
- [45] Hu G, Cateto C, Pu Y, Samuel R, Ragauskas AJ. Structural characterization of switchgrass lignin after ethanol organosolv pretreatment. *Energy Fuels* 2011;26:740–5.
- [46] Fortin M, Mohadjer Beromi M, Lai A, Tarves PC, Mullen CA, Boateng AA, et al. Structural analysis of pyrolytic lignins isolated from switchgrass fast-pyrolysis oil. *Energy Fuels* 2015;29:8017–26.
- [47] Mullen CA, Boateng AA. Characterization of water insoluble solids isolated from various biomass fast pyrolysis oils. *J Anal Appl Pyrolysis* 2011;90:197–203.
- [48] Gayubo A, Valle B, Aguayo A, Olazar M, Bilbao J. Pyrolytic lignin removal for the valorization of biomass pyrolysis crude bio-oil by catalytic transformation. *J Chem Technol Biotechnol* 2010;85:132–44.
- [49] Wang C, Li M, Fang Y. Upgrading of pyrolytic lignin into hexamethylbenzene with high purity: demonstration of “All-to-One” biochemical production strategy in thermo-chemical conversion. *Green Chem* 2019.
- [50] Qu W, Xue Y, Gao Y, Rover M, Bai X. Repolymerization of pyrolytic lignin for producing carbon fiber with improved properties. *Biomass-Bioenergy* 2016;95:19–26.
- [51] Bridgwater AV. Review of fast pyrolysis of biomass and product upgrading. *Biomass-Bioenergy* 2012;38:68–94.
- [52] Barth T, Kleinert M. Motor fuels from biomass pyrolysis. *Chem Eng Technol* 2008;31:773–81.
- [53] Gardner DJ, Schult TP, McGinnis GD. The pyrolytic behavior of selected lignin preparations. *J Wood Chem Technol* 1985;5:85–110.

- [54] Serio MA, Charpenay S, Bassilakis R, Solomon PR. Measurement and modeling of lignin pyrolysis. *Biomass- Bioenergy* 1994;7:107–24.
- [55] Patwardhan PR, Brown RC, Shanks BH. Understanding the fast pyrolysis of lignin. *ChemSusChem* 2011;4:1629–36.
- [56] Yang H, Yan R, Chen H, Lee DH, Zheng C. Characteristics of hemicellulose, cellulose and lignin pyrolysis. *Fuel* 2007;86:1781–8.
- [57] Shen Y, Yoshikawa K. Recent progresses in catalytic tar elimination during biomass gasification or pyrolysis—A review. *Renew Sustain Energy Rev* 2013;21:371–92.
- [58] Ferdous D, Dalai AK, Bej SK, Thring RW. Pyrolysis of lignins: experimental and kinetics studies. *Energy Fuels* 2002;16:1405–12.
- [59] Evans RJ, Milne TA. Molecular characterization of the pyrolysis of biomass. *Energy Fuels* 1987;1:123–37.
- [60] Kawamoto H, Horigoshi S, Saka S. Pyrolysis reactions of various lignin model dimers. *J Wood Sci* 2007;53:168–74.
- [61] Mullen CA, Boateng AA. Catalytic pyrolysis-GC/MS of lignin from several sources. *Fuel Process Technol* 2010;91:1446–58.
- [62] Kawamoto H. Lignin pyrolysis reactions. *J Wood Sci* 2017;63:117–32.
- [63] Kotake T, Kawamoto H, Saka S. Mechanisms for the formation of monomers and oligomers during the pyrolysis of a softwood lignin. *J Anal Appl Pyrolysis* 2014;105:309–16.
- [64] Kotake T, Kawamoto H, Saka S. Pyrolytic formation of monomers from hardwood lignin as studied from the reactivities of the primary products. *J Anal Appl Pyrolysis* 2015;113:57–64.
- [65] Asmadi M, Kawamoto H, Saka S. Thermal reactions of guaiacol and syringol as lignin model aromatic nuclei. *J Anal Appl Pyrolysis* 2011;92:88–98.
- [66] Asmadi M, Kawamoto H, Saka S. Gas- and solid/liquid-phase reactions during pyrolysis of softwood and hardwood lignins. *J Anal Appl Pyrolysis* 2011;92:417–25.
- [67] Ledesma EB, Marsh ND, Sandrowitz AK, Wornat MJ. An experimental study on the thermal decomposition of catechol. *Proc Combust Inst* 2002;29:2299–306.
- [68] Asmadi M, Kawamoto H, Saka S. Thermal reactivities of catechols/pyrogallols and cresols/xyleneols as lignin pyrolysis intermediates. *J Anal Appl Pyrolysis* 2011;92:76–87.
- [69] Hosoya T, Kawamoto H, Saka S. Role of methoxyl group in char formation from lignin-related compounds. *J Anal Appl Pyrolysis* 2009;84:79–83.
- [70] Windt M, Meier D, Marsman JH, Heeres HJ, de Koning S. Micro-pyrolysis of technical lignins in a new modular rig and product analysis by GC-MS/FID and GC × GC-TOFMS/FID. *J Anal Appl Pyrolysis* 2009;85:38–46.
- [71] Santana JA, Carvalho WS, Ataíde CH. Catalytic effect of ZSM-5 zeolite and HY-340 niobic acid on the pyrolysis of industrial kraft lignins. *Ind Crops Prod* 2018;111:126–32.
- [72] Li X, Su L, Wang Y, Yu Y, Wang C, Li X, et al. Catalytic fast pyrolysis of Kraft lignin with HZSM-5 zeolite for producing aromatic hydrocarbons. *Front Environ Sci Eng* 2012;6:295–303.
- [73] Shen D, Zhao J, Xiao R, Gu S. Production of aromatic monomers from catalytic pyrolysis of black-liquor lignin. *J Anal Appl Pyrolysis* 2015;111:47–54.
- [74] Ma Z, van Bokhoven JA. Deactivation and regeneration of H-USY zeolite during lignin catalytic fast pyrolysis. *ChemCatChem* 2012;4:2036–44.
- [75] Ma Z, Custodis V, van Bokhoven JA. Selective deoxygenation of lignin during catalytic fast pyrolysis. *Catal Sci Technol* 2014;4:766.
- [76] Goñi MA, Montgomery S. Alkaline CuO oxidation with a microwave digestion system: lignin analyses of geochemical samples. *Anal Chem* 2000;72:3116–21.
- [77] de la Hoz A, Diaz-Ortiz A, Moreno A. Microwaves in organic synthesis. Thermal and non-thermal microwave effects. *Chem Soc Rev* 2005;34:164–78.
- [78] Beneroso D, Monti T, Kostas ET, Robinson J. Microwave pyrolysis of biomass for bio-oil production: scalable processing concepts. *Chem Eng J* 2017;316:481–98.
- [79] Yunpu W, Leilei DAI, Liangliang FAN, Shaoqi S, Yuhuan LIU, Roger R. Review of microwave-assisted lignin conversion for renewable fuels and chemicals. *J Anal Appl Pyrolysis* 2016;119:104–13.
- [80] Lam SS, Mahari WAW, Jusoh A, Chong CT, Lee CL, Chase HA. Pyrolysis using microwave absorbents as reaction bed: an improved approach to transform used frying oil into biofuel product with desirable properties. *J Clean Prod* 2017;147:263–72.
- [81] Duan D, Wang Y, Dai L, Ruan R, Zhao Y, Fan L, et al. Ex-situ catalytic co-pyrolysis of lignin and polypropylene to upgrade bio-oil quality by microwave heating. *Bioresour Technol* 2017;241:207–13.
- [82] Liew RK, Chai C, Yek PNY, Phang XY, Chong MY, Nam WL, et al. Innovative production of highly porous carbon for industrial effluent remediation via microwave vacuum pyrolysis plus sodium-potassium hydroxide mixture activation. *J Clean Prod* 2019;208:1436–45.
- [83] Dai L, Fan L, Duan D, Ruan R, Wang Y, Liu Y, et al. Production of hydrocarbon-rich bio-oil from soapstock via fast microwave-assisted catalytic pyrolysis. *J Anal Appl Pyrolysis* 2017;125:356–62.
- [84] Zhu G, Jin D, Zhao L, Ouyang X, Chen C, Qiu X. Microwave-assisted selective cleavage of CαCβ bond for lignin depolymerization. *Fuel Process Technol* 2017;161:155–61.
- [85] Duan D, Ruan R, Wang Y, Liu Y, Dai L, Zhao Y, et al. Microwave-assisted acid pretreatment of alkali lignin: effect on characteristics and pyrolysis behavior. *Bioresour Technol* 2018;251:57–62.
- [86] Merino O, Fundora-Galano G, Luque R, Martínez-Palou R. Understanding microwave-assisted lignin solubilization in protic ionic liquids with multiaromatic imidazolium cations. *ACS Sustain Chem Eng* 2018;6:4122–9.
- [87] Mazo P, Estenoz D, Sponton M, Rios L. Kinetics of the Transesterification of castor oil with maleic anhydride using conventional and microwave heating. *J Am Oil Chem Soc* 2012;89:1355–61.
- [88] Xue BL, Wen JL, Sun RC. Producing lignin-based polyols through microwave-assisted liquefaction for rigid polyurethane foam production. *Materials* 2015;8:586–99.
- [89] Gosz K, Kosmela P, Hejna A, Gajowicz G, Piszczyk Ł. Biopolyols obtained via microwave-assisted liquefaction of lignin: structure, rheological, physical and thermal properties. *Wood Sci Technol* 2018;52:599–617.
- [90] Wang H, Tucker M, Ji Y. Recent development in chemical depolymerization of lignin: a review. *J Appl Chem* 2013;2013:1–9.
- [91] Hewson WB, Hibbert H. Studies on lignin and related compounds. LXV. re-ethanolization of isolated lignins. *J Am Chem Soc* 1943;65:1173–6.
- [92] Mahmood N, Yuan Z, Schmidt J, Xu CC. Hydrolytic depolymerization of hydrolysis lignin: effects of catalysts and solvents. *Bioresour Technol* 2015;190:416–9.
- [93] Jia S, Cox BJ, Guo X, Zhang ZC, Ekerdt JG. Cleaving the β-O-4 bonds of lignin model compounds in an acidic ionic liquid, 1-H-3-methylimidazolium chloride: an optional strategy for the degradation of lignin. *ChemSusChem* 2010;3:1078–84.
- [94] Chen L, Dou J, Ma Q, Li N, Wu R, Bian H, et al. Rapid and near-complete dissolution of wood lignin at < />= 80 degrees C by a recyclable acid hydrotrope. *Sci Adv* 2017;3:e1701735.
- [95] Forsythe WG, Garrett MD, Hardacre C, Nieuwenhuyzen M, Sheldrake GN. An efficient and flexible synthesis of model lignin oligomers. *Green Chem* 2013;15:3031.
- [96] Thring RW. Alkaline degradation of ALCELL® lignin. *Biomass- Bioenergy* 1994;7:125–30.
- [97] Yuan Z, Cheng S, Leitch M, Xu CC. Hydrolytic degradation of alkaline lignin in hot-compressed water and ethanol. *Bioresour Technol* 2010;101:9308–13.
- [98] Evans L, Littlewolf A, Lopez M, Miller J. Batch microreactor studies of base catalyzed lignin depolymerization in alcohol solvents. Albuquerque, NM, and Livermore, CA: Sandia National Laboratories; 1999.
- [99] Yoshikawa T, Yagi T, Shinohara S, Fukunaga T, Nakasaka Y, Tago T, et al. Production of phenols from lignin via depolymerization and catalytic cracking. *Fuel Process Technol* 2013;108:69–75.
- [100] Deuss PJ, Scott M, Tran F, Westwood NJ, de Vries JG, Barta K. Aromatic monomers by in situ conversion of reactive intermediates in the acid-catalyzed depolymerization of lignin. *J Am Chem Soc* 2015;137:7456–67.
- [101] Gierer J. Chemistry of delignification. *Wood Sci Technol* 1985;19:289–312.
- [102] Knill CJ, Kennedy JF. Degradation of cellulose under alkaline conditions. *Carbohydr Polym* 2003;51:281–300.
- [103] Jin Y, Ruan X, Cheng X, Lu Q. Liquefaction of lignin by polyethyleneglycol and glycerol. *Bioresour Technol* 2011;102:3581–3.
- [104] Wang X, Rinaldi R. A route for lignin and bio-oil conversion: dehydroxylation of phenols into arenes by catalytic tandem reactions. *Angew Chem Int Ed* 2013;52:11499–503.
- [105] Paola F, Roberto R. Catalytic Biorefining of plant biomass to non-pyrolytic lignin bio-oil and carbohydrates through hydrogen transfer reactions. *Angew Chem Int Ed* 2014;53:8634–9.
- [106] Jasiukaitė E, Kunaver M, Crestini C. Lignin behaviour during wood liquefaction—characterization by quantitative 31P, 13C NMR and size-exclusion chromatography. *Catal Today* 2010;156:23–30.
- [107] Karagoz S, Bhaskar T, Muto A, Sakata Y. Hydrothermal upgrading of biomass: effect of K₂CO₃ concentration and biomass/water ratio on products distribution. *Bioresour Technol* 2006;97:90–8.
- [108] Lavoie JM, Bare W, Bilodeau M. Depolymerization of steam-treated lignin for the production of green chemicals. *Bioresour Technol* 2011;102:4917–20.
- [109] Forchheim D, Gasson JR, Hornung U, Kruse A, Barth T. Modeling the lignin degradation kinetics in an ethanol/formic acid solvolysis approach. Part 2. Validation and transfer to variable conditions. *Ind Eng Chem Res* 2012;51:15053–63.
- [110] Weiyin X, MS J, K AP, W JC. Depolymerization and hydrodeoxygenation of switchgrass lignin with formic acid. *ChemSusChem* 2012;5:667–75.
- [111] Song Q, Wang F, Xu J. Hydrogenolysis of lignosulfonate into phenols over heterogeneous nickel catalysts. *Chem Commun* 2012;48:7019–21.
- [112] Song Q, Wang F, Cai J, Wang Y, Zhang J, Yu W, et al. Lignin depolymerization (LDP) in alcohol over nickel-based catalysts via a fragmentation-hydrogenolysis process. *Energy Environ Sci* 2013;6:994.
- [113] Zhang J, Teo J, Chen X, Asakura H, Tanaka T, Teramura K, et al. A series of NiM (M = Ru, Rh, and Pd) bimetallic catalysts for effective lignin hydrogenolysis in water. *ACS Catal* 2014;4:1574–83.
- [114] Zhang J-w, Cai Y, Lu G-p, Cai C. Facile and selective hydrogenolysis of β-O-4 linkages in lignin catalyzed by Pd-Ni bimetallic nanoparticles supported on ZrO₂. *Green Chem* 2016;18:6229–35.
- [115] Zhang J, Asakura H, van Rijn J, Yang J, Duchesne P, Zhang B, et al. Highly efficient, NiAu-catalyzed hydrogenolysis of lignin into phenolic chemicals. *Green Chem* 2014;16:2432–7.
- [116] Grilc M, Likozar B, Levec J. Hydrodeoxygenation and hydrocracking of solvolyzed lignocellulosic biomass by oxide, reduced and sulphide form of NiMo, Ni, Mo and Pd catalysts. *Appl Catal B* 2014;150:275–87.
- [117] Molinari V, Giordano C, Antonietti M, Esposito D. Titanium nitride-nickel nanocomposite as heterogeneous catalyst for the hydrogenolysis of aryl ethers. *J Am Chem Soc* 2014;136:1758–61.
- [118] Zhai Y, Li C, Xu G, Ma Y, Liu X, Zhang Y. Depolymerization of lignin via a non-precious Ni-Fe alloy catalyst supported on activated carbon. *Green Chem* 2017;19:1895–903.
- [119] Kim J-Y, Park SY, Choi I-G, Choi JW. Evaluation of Ru x Ni 1-x/SBA-15 catalysts for depolymerization features of lignin macromolecule into monomeric phenols. *Chem Eng J* 2018;336:640–8.
- [120] García-Morales NG, García-Cerda LA, Puente-Urbina BA, Blanco-Jerez LM, Antaño-López R, Castañeda-Zaldívar F. Electrochemical glucose oxidation using

- glassy carbon electrodes modified with Au-Ag nanoparticles: influence of Ag content. *J Nanomater* 2015;2015:2.
- [121] Shuai L, Luterbacher J. Organic solvent effects in biomass conversion reactions. *ChemSusChem* 2016;9:133–55.
- [122] Qiu S, Li M, Huang Y, Fang Y. Catalytic hydrotreatment of Kraft lignin over NiW/SiC: effective depolymerization and catalyst regeneration. *Ind Eng Chem Res* 2018;57:2023–30.
- [123] Yan N, Zhao C, Dyson PJ, Wang C, Liu LT, Kou Y. Selective degradation of wood lignin over noble-metal catalysts in a two-step process. *ChemSusChem* 2008;1:626–9.
- [124] Li S, Li W, Zhang Q, Shu R, Wang H, Xin H, et al. Lignin-first depolymerization of native corn stover with an unsupported MoS₂ catalyst. *RSC Adv* 2018;8:1361–70.
- [125] Zhang X, Tang W, Zhang Q, Li Y, Chen L, Xu Y, et al. Production of hydrocarbon fuels from heavy fraction of bio-oil through hydrodeoxygenative upgrading with Ru-based catalyst. *Fuel* 2018;215:825–34.
- [126] Shu R, Xu Y, Ma L, Zhang Q, Wang C, Chen Y. Controllable production of guaiacols and phenols from lignin depolymerization using Pd/C catalyst cooperated with metal chloride. *Chem Eng J* 2018.
- [127] Ye Y, Zhang Y, Fan J, Chang J. Selective production of 4-ethylphenolics from lignin via mild hydrogenolysis. *Bioresour Technol* 2012;118:648–51.
- [128] Huddleston JG, Visser AE, Reichert WM, Willauer HD, Broker GA, Rogers RD. Characterization and comparison of hydrophilic and hydrophobic room temperature ionic liquids incorporating the imidazolium cation. *Green Chem* 2001;3:156–64.
- [129] Wang H, Block LE, Rogers RD. Catalytic conversion of biomass in ionic liquids. 2014.
- [130] Zakzeski J, Buijninx PC, Jongerius AL, Weckhuysen BM. The catalytic valorization of lignin for the production of renewable chemicals. *Chem Rev* 2010;110:3552–99.
- [131] Stärk K, Taccardi N, Bösmann A, Wasserscheid P. Oxidative depolymerization of lignin in ionic liquids. *ChemSusChem* 2010;3:719–23.
- [132] Zakzeski J, Jongerius AL, Weckhuysen BM. Transition metal catalyzed oxidation of alcell lignin, soda lignin, and lignin model compounds in ionic liquids. *Green Chem* 2010;12:1225–36.
- [133] Liu S, Shi Z, Li L, Yu S, Xie C, Song Z. Process of lignin oxidation in an ionic liquid coupled with separation. *RSC Adv* 2013;3:5789–93.
- [134] Zakzeski J, Buijninx PC, Weckhuysen BM. In situ spectroscopic investigation of the cobalt-catalyzed oxidation of lignin model compounds in ionic liquids. *Green Chem* 2011;13:671–80.
- [135] Yang Y, Fan H, Meng Q, Zhang Z, Yang G, Han B. Ionic liquid [OMIm][OAc] directly inducing oxidation cleavage of the β-O-4 bond of lignin model compounds. *Chem Commun* 2017;53:8850–3.
- [136] Dier TKF, Rauber D, Durnea D, Hempelmann R, Volmer DA. Sustainable electrochemical depolymerization of lignin in reusable ionic liquids. *Sci Rep* 2017;7:5041.
- [137] Cocero MJ, Cabeza Á, Abad N, Adamovic T, Vaquerizo L, Martínez CM, et al. Understanding biomass fractionation in subcritical and supercritical water. *J Supercrit Fluids* 2017.
- [138] Saisu M, Sato T, Watanabe M, Adschiri T, Arai K. Conversion of lignin with supercritical water – phenol mixtures. *Energy Fuels* 2003;17:922–8.
- [139] Sasaki M, Goto M. Recovery of phenolic compounds through the decomposition of lignin in near and supercritical water. *Chem Eng Process* 2008;47:1609–19.
- [140] Yong TL-K, Matsumura Y. Kinetic analysis of lignin hydrothermal conversion in sub-and supercritical water. *Ind Eng Chem Res* 2013;52:5626–39.
- [141] Fang Z, Sato T, Smith Jr. RL, Inomata H, Arai K, Kozinski JA. Reaction chemistry and phase behavior of lignin in high-temperature and supercritical water. *Bioresour Technol* 2008;99:3424–30.
- [142] Aida TM, Sato T, Sekiguchi G, Adschiri T, Arai K. Extraction of Taiheiyō coal with supercritical water–phenol mixtures. *Fuel* 2002;81:1453–61.
- [143] Okuda K, Umetsu M, Takami S, Adschiri T. Disassembly of lignin and chemical recovery—rapid depolymerization of lignin without char formation in water–phenol mixtures. *Fuel Process Technol* 2004;85:803–13.
- [144] Paterson RJ. Lignin: properties and applications in biotechnology and bioenergy. Nova Science Publishers; 2012.
- [145] Dorrestijn E, Kranenburg M, Poinot D, Mulder P. Lignin depolymerization in hydrogen-donor solvents. *Holzforschung* 1999;53:611–6.
- [146] Cheng S, D'cruz I, Wang M, Leitch M, Xu C. Highly efficient liquefaction of woody biomass in hot-compressed alcohol – water co-solvents. *Energy Fuels* 2010;24:4659–67.
- [147] Rahimi A, Ulbrich A, Coon JJ, Stahl SS. Formic-acid-induced depolymerization of oxidized lignin to aromatics. *Nature* 2014;515:249–52.
- [148] Das L, Kolar P, Sharma-Shivappa R, Classen JJ, Osborne JA. Catalytic valorization of lignin using niobium oxide. *Waste Biomass- Valor* 2017;8:2673–80.
- [149] Nyamunda BC, Chigondo F, Moyo M, Guyo U, Shumba M, Nharingo T. Hydrogen peroxide as an oxidant for organic reactions. *J At Mol* 2013;3:23.
- [150] Crestini C, Caponi MC, Argyropoulos DS, Saladino R. Immobilized methyltrioxo rhenium (MTO)/H₂O₂ systems for the oxidation of lignin and lignin model compounds. *Bioorg Med Chem* 2006;14:5292–302.
- [151] Jennings JA, Parkin S, Munson E, Delaney SP, Calahan JL, Isaacs M, et al. Regioselective Baeyer–Villiger oxidation of lignin model compounds with tin beta zeolite catalyst and hydrogen peroxide. *RSC Adv* 2017;7:25987–97.
- [152] Zhang C, Li H, Lu J, Zhang X, MacArthur KE, Heggen M, et al. Promoting lignin depolymerization and restraining the condensation via an oxidation – hydrogenation strategy. *ACS Catal* 2017;7:3419–29.
- [153] Hasegawa I, Inoue Y, Muranaka Y, Yasukawa T, Mae K. Selective production of organic acids and depolymerization of lignin by hydrothermal oxidation with diluted hydrogen peroxide. *Energy Fuels* 2011;25:791–6.
- [154] Wang Q, Tian D, Hu J, Shen F, Yang G, Zhang Y, et al. Fates of hemicellulose, lignin and cellulose in concentrated phosphoric acid with hydrogen peroxide (PHP) pretreatment. *RSC Adv* 2018;8:12714–23.
- [155] Fernández-Rodríguez J, Erdocia X, de Hoyos PL, Alriols MG, Labidi J. Small phenolic compounds production from kraft black liquor by lignin depolymerization with different catalytic agents. *Chem Eng* 2017:57.
- [156] Qiao X, Zhao C, Shao Q, Hassan M. Structural characterization of corn stover lignin after hydrogen peroxide presoaking prior to ammonia fiber expansion pretreatment. *Energy Fuels* 2018.
- [157] Mackenzie AK, Naas AE, Kracun SK, Schuckel J, Fangel JU, Agger JW, et al. A polysaccharide utilization locus from an uncultured bacteroidetes phylotype suggests ecological adaptation and substrate versatility. *Appl Environ Microbiol* 2015;81:187–95.
- [158] Wang J, Cao F, Su E, Zhao L, Qin W. Improvement of animal feed additives of Ginkgo leaves through solid-state fermentation using *Aspergillus niger*. *Int J Biol Sci* 2018;14:736–47.
- [159] Wang J, Cao F, Su E, Wu C, Zhao L, Ying R. Improving flavonoid extraction from Ginkgo biloba leaves by prefermentation processing. *J Agric Food Chem* 2013;61:5783–91.
- [160] Fuchs G, Boll M, Heider J. Microbial degradation of aromatic compounds—from one strategy to four. *Nat Rev Microbiol* 2011;9:803.
- [161] Ahmad M, Roberts JN, Hardiman EM, Singh R, Eltis LD, Bugg TD. Identification of DypB from *Rhodococcus jostii* RHA1 as a lignin peroxidase. *Biochemistry* 2011;50:5096–107.
- [162] Sainsbury PD, Mineyeva Y, Mycroft Z, Bugg TD. Chemical intervention in bacterial lignin degradation pathways: development of selective inhibitors for intradiol and extradiol catechol dioxygenases. *Bioorg Chem* 2015;60:102–9.
- [163] Seto M, Masai E, Ida M, Hatta T, Kimbara K, Fukuda M, et al. Multiple polychlorinated biphenyl transformation systems in the gram-positive bacterium *Rhodococcus* sp. strain RHA1. *Appl Environ Microbiol* 1995;61:4510–3.
- [164] Kitagawa W, Miyauchi K, Masai E, Fukuda M. Cloning and characterization of benzoate catabolic genes in the gram-positive polychlorinated biphenyl degrader *Rhodococcus* sp. strain RHA1. *J Bacteriol* 2001;183:6598–606.
- [165] Sainsbury PD, Hardiman EM, Ahmad M, Otani H, Seghezzi N, Eltis LD, et al. Breaking down lignin to high-value chemicals: the conversion of lignocellulose to vanillin in a gene deletion mutant of *Rhodococcus jostii* RHA1. *ACS Chem Biol* 2013;8:2151–6.
- [166] Salvachúa D, Karp EM, Nimlos CT, Vardon DR, Beckham GT. Towards lignin consolidated bioprocessing: simultaneous lignin depolymerization and product generation by bacteria. *Green Chem* 2015;17:4951–67.
- [167] Linger JG, Vardon DR, Guarneri MT, Karp EM, Hunsinger GB, Franden MA, et al. Lignin valorization through integrated biological funneling and chemical catalysis. *Proc Natl Acad Sci USA* 2014;111:12013–8.
- [168] Xu Z, Qin L, Cai M, Hua W, Jin M. Biodegradation of kraft lignin by newly isolated *Klebsiella pneumoniae*, *Pseudomonas putida*, and *Ochrobactrum tritici* strains. *Environ Sci Pollut Res Int* 2018;25:14171–81.
- [169] Martínez-García E, Nikel PI, Aparicio T, de Lorenzo V. *Pseudomonas* 2.0: genetic upgrading of *P. putida* KT2440 as an enhanced host for heterologous gene expression. *Microb Cell Fact* 2014;13:159.
- [170] Lieder S, Nikel PI, de Lorenzo V, Takors R. Genome reduction boosts heterologous gene expression in *Pseudomonas putida*. *Microb Cell Fact* 2015;14:23.
- [171] Olivera ER, Carnicero D, Jodra R, Minambres B, Garcia B, Abraham GA, et al. Genetically engineered *Pseudomonas*: a factory of new bioplastics with broad applications. *Environ Microbiol* 2001;3:612–8.
- [172] Vardon DR, Franden MA, Johnson CW, Karp EM, Guarneri MT, Linger JG, et al. Adipic acid production from lignin. *Energy Environ Sci* 2015;8:617–28.
- [173] Johnson CW, Beckham GT. Aromatic catabolic pathway selection for optimal production of pyruvate and lactate from lignin. *Metab Eng* 2015;28:240–7.
- [174] Davis JR, Goodwin LA, Woyke T, Teshima H, Bruce D, Dettler C, et al. Genome sequence of *Amycolatopsis* sp. strain ATCC 39116, a plant biomass-degrading actinomycete. *J Bacteriol* 2012;194:2396–7.
- [175] Achterholt S, Priefert H, Steinbuechel A. Identification of *Amycolatopsis* sp. strain HR167 genes, involved in the bioconversion of ferulic acid to vanillin. *Appl Microbiol Biotechnol* 2000;54:799–807.
- [176] Fleige C, Hansen G, Kroll J, Steinbuechel A. Investigation of the *Amycolatopsis* sp. strain ATCC 39116 vanillin dehydrogenase and its impact on the biotechnical production of vanillin. *Appl Environ Microbiol* 2013;79:81–90.
- [177] Barton N, Horbal L, Starck S, Kohlstedt M, Luzhetskyy A, Wittmann C. Enabling the valorization of guaiacol-based lignin: integrated chemical and biochemical production of *cis*, *cis*-muconic acid using metabolically engineered *Amycolatopsis* sp ATCC 39116. *Metab Eng* 2018;45:200–10.
- [178] Ahmad M, Taylor CR, Pink D, Burton K, Eastwood D, Bending GD, et al. Development of novel assays for lignin degradation: comparative analysis of bacterial and fungal lignin degraders. *Mol Biosyst* 2010;6:815–21.
- [179] Beckham GT, Johnson CW, Karp EM, Salvachúa D, Vardon DR. Opportunities and challenges in biological lignin valorization. *Curr Opin Biotechnol* 2016;42:40–53.
- [180] Reddy CA. The potential for white-rot fungi in the treatment of pollutants. *Curr Opin Biotechnol* 1995;6:320–8.
- [181] Asgher M, Bhatti HN, Ashraf M, Legge RL. Recent developments in biodegradation of industrial pollutants by white rot fungi and their enzyme system. *Biodegradation* 2008;19:771.
- [182] Nizami AS, Korres NE, Murphy JD. Review of the integrated process for the production of grass biomethane. *Environ Sci Technol* 2009;43:8496–508.
- [183] Shi J, Sharma-Shivappa RR, Chinn M, Howell N. Effect of microbial pretreatment on enzymatic hydrolysis and fermentation of cotton stalks for ethanol production.

- Biomass- Bioenergy 2009;33:88–96.
- [184] Zhi Z, Wang H. White-rot fungal pretreatment of wheat straw with *Phanerochaete chrysosporium* for biohydrogen production: simultaneous saccharification and fermentation. *Bioprocess Biosyst Eng* 2014;37:1447–58.
- [185] Rytioja J, Hilden K, Yuzon J, Hatakka A, de Vries RP, Makela MR. Plant-poly-saccharide-degrading enzymes from Basidiomycetes. *Microbiol Mol Biol Rev* 2014;78:614–49.
- [186] Pérez J, Munoz-Dorado J, de la Rubia T, Martínez J. Biodegradation and biological treatments of cellulose, hemicellulose and lignin: an overview. *Int Microbiol* 2002;5:53–63.
- [187] Sharari M, Latibari AJ, Guillet A, Arousseau M, Mouhamadou B, Rafeiee G, et al. Application of the white rot fungus *Phanerochaete chrysosporium* in biotreatment of bagasse effluent. *Biodegradation* 2011;22:421–30.
- [188] Kocsag CI, Eastwood D, Collis AE, Coles SR, Clark AJ, Kirwan K, et al. Extracting valuable compounds from straw degraded by *Pleurotus ostreatus*. *Resour Conserv Recycl* 2012;59:14–22.
- [189] Baltierra-Trejo E, Sanchez-Yanez JM, Buenrostro-Delgado O, Marquez-Benavides L. Production of short-chain fatty acids from the biodegradation of wheat straw lignin by *Aspergillus fumigatus*. *Bioresour Technol* 2015;196:418–25.
- [190] Xie S, Qin X, Cheng Y, Laskar D, Qiao W, Sun S, et al. Simultaneous conversion of all cell wall components by an oleaginous fungus without chemi-physical pretreatment. *Green Chem* 2015;17:1657–67.
- [191] Fonseca MI, Molina MA, Winnik DL, Busi MV, Farina JI, Villalba LL, et al. Isolation of a laccase-coding gene from the lignin-degrading fungus *Phlebia brevispora* BAFC 633 and heterologous expression in *Pichia pastoris*. *J Appl Microbiol* 2018;124:1454–68.
- [192] Jin W, Li J, Feng H, You S, Zhang L, Norvinyeku J, et al. Importance of a Laccase Gene (Lcc1) in the development of *Ganoderma tsugae*. *Int J Mol Sci* 2018;19:471.
- [193] Kinnunen A, Majjala P, Järvinen P, Hatakka A. Improved efficiency in screening for lignin-modifying peroxidases and laccases of basidiomycetes. *Curr Biotechnol* 2017;6:105–15.
- [194] Mathieu Y, Gelhaye E, Dumarcay S, Gérardin P, Harvengt L, Buée M. Selection and validation of enzymatic activities as functional markers in wood biotechnology and fungal ecology. *J Microbiol Methods* 2013;92:157–63.
- [195] Marinović M, Nousiainen P, Dilokpimol A, Kontro J, Moore R, Sipilä J, et al. Selective cleavage of lignin β -O-4 aryl ether bond by β -etherase of the white-rot fungus *Dichomitus squalens*. *ACS Sustain Chem Eng* 2018;6:2878–2.
- [196] Munk L, Sitarz AK, Kalyani DC, Mikkelsen JD, Meyer AS. Can laccases catalyze bond cleavage in lignin? *Biotechnol Adv* 2015;33:13–24.
- [197] Zhang YH. Production of biofuels and biochemicals by in vitro synthetic biosystems: opportunities and challenges. *Biotechnol Adv* 2015;33:1467–83.
- [198] Picart P, Domínguez de María P, Schallmey A. From gene to biorefinery: microbial β -etherases as promising biocatalysts for lignin valorization. *Front Microbiol* 2015;6:916.
- [199] Leonowicz A, Cho NS, Luterek J, Wilkolazka A, Wojtas-Wasilewska M, Matuszewska A, et al. Fungal laccase: properties and activity on lignin. *J Basic Microbiol* 2001;41:185–227.
- [200] Gianfreda L, Xu F, Bollag J-M. Laccases: a useful group of oxidoreductive enzymes. *Bioremediat J* 1999;3:1–26.
- [201] Bourbonnais R, Paice MG. Oxidation of non-phenolic substrates. An expanded role for laccase in lignin biodegradation. *FEBS Lett* 1990;267:99–102.
- [202] Hilgers RJ, Vincken J-P, Gruppen H, Kabel MA. Laccase/mediator systems: their reactivity towards phenolic lignin structures. *ACS Sustain Chem Eng* 2018.
- [203] Camarero S, Garcia O, Vidal T, Colom J, del Ruo JC, Gutiérrez A, et al. Efficient bleaching of non-wood high-quality paper pulp using laccase-mediator system. *Enzym Microb Technol* 2004;35:113–20.
- [204] Lim J, Sana B, Krishnan R, Seayad J, Ghadessy FJ, Jana S, et al. Laccase-catalyzed synthesis of low-molecular-weight lignin-like oligomers and their application as UV-blocking materials. *Chem Asian J* 2018;13:284–91.
- [205] Li Z, Zhang J, Qin L, Ge Y. Enhancing antioxidant performance of lignin by enzymatic treatment with laccase. *ACS Sustain Chem Eng* 2018;6:2591–5.
- [206] Chen Q, Marshall MN, Geib SM, Tien M, Richard TL. Effects of laccase on lignin depolymerization and enzymatic hydrolysis of ensiled corn stover. *Bioresour Technol* 2012;117:186–92.
- [207] Thurston CF. The structure and function of fungal laccases. *Microbiol* 1994;140:19–26.
- [208] Martínez D, Larrondo LF, Putnam N, Gelpke MD, Huang K, Chapman J, et al. Genome sequence of the lignocellulose degrading fungus *Phanerochaete chrysosporium* strain RP78. *Nat Biotechnol* 2004;22:695–700.
- [209] Datta R, Kelkar A, Baraniya D, Molaei A, Moullick A, Meena RS, et al. Enzymatic degradation of lignin in soil: a review. *Sustainability* 2017;9:1163.
- [210] Wong DW. Structure and action mechanism of ligninolytic enzymes. *Appl Biochem Biotechnol* 2009;157:174–209.
- [211] Sigoiillot J-C, Berrin J-G, Bey M, Lesage-Meessen L, Levasseur A, Lomascolo A, et al. Fungal strategies for lignin degradation. *Adv Bot Res* 2012;263–308.
- [212] Zhang Z, Xia L, Wang F, Lv P, Zhu M, Li J, et al. Lignin degradation in corn stalk by combined method of H₂O₂ hydrolysis and *Aspergillus oryzae* CGMCC5992 liquid-state fermentation. *Biotechnol Biofuels* 2015;8:183.
- [213] Vandana T, Rao RG, Kumar SA, Swaraj S, Manpal S. Enhancing production of lignin peroxidase from white rot fungi employing statistical optimization and evaluation of its potential in delignification of crop residues. *Int J Curr Microbiol Appl Sci* 2018;7:2599–621.
- [214] Hofrichter M. Lignin conversion by manganese peroxidase (MnP). *Enzym Microb Technol* 2002;30:454–66.
- [215] Guillén F, Martínez MJ, Gutiérrez A, Del Río J. Biodegradation of lignocelluloses: microbial, chemical, and enzymatic aspects of the fungal attack of lignin. *Int Microbiol* 2005;8:195–204.
- [216] Jayasinghe PA, Hettiaratchi JP, Mehrotra AK, Kumar S. Effect of enzyme additions on methane production and lignin degradation of landfilled sample of municipal solid waste. *Bioresour Technol* 2011;102:4633–7.
- [217] Hettiaratchi JP, Jayasinghe PA, Bartholameuz EM, Kumar S. Waste degradation and gas production with enzymatic enhancement in anaerobic and aerobic landfill bioreactors. *Bioresour Technol* 2014;159:433–6.
- [218] Rothschild N, Levkowitz A, Hadar Y, Dosoretz CG. Manganese deficiency can replace high oxygen levels needed for lignin peroxidase formation by *Phanerochaete chrysosporium*. *Appl Environ Microbiol* 1999;65:483–8.
- [219] Kirk TK, Cullen D. *Enzymology and molecular genetics of wood degradation by white-rot fungi*. New York: Environmentally friendly technologies for the pulp and paper industry Wiley; 1998. p. 273–307.
- [220] Hammel KE, Jensen Jr. KA, Mozuch MD, Landucci LL, Tien M, Pease EA. Ligninolysis by a purified lignin peroxidase. *J Biol Chem* 1993;268:12274–81.
- [221] Wariishi H, Valli K, Gold MH. In vitro depolymerization of lignin by manganese peroxidase of *Phanerochaete chrysosporium*. *Biochem Biophys Res Commun* 1991;176:269–75.
- [222] Moreira PR, Almeida-Vara E, Malcata FX, Duarte JC. Lignin transformation by a versatile peroxidase from a novel *Bjerkandera* sp. strain. *Int Biodeterior Biodegrad* 2007;59:234–8.
- [223] Ruiz-Dueñas FJ, Morales M, García E, Miki Y, Martínez MJ, Martínez AT. Substrate oxidation sites in versatile peroxidase and other basidiomycete peroxidases. *J Exp Bot* 2008;60:441–52.
- [224] Camarero S, Sarkar S, Ruiz-Dueñas FJ, Martínez MaJ, Martínez ÁT. Description of a versatile peroxidase involved in the natural degradation of lignin that has both manganese peroxidase and lignin peroxidase substrate interaction sites. *J Biol Chem* 1999;274:10324–30.
- [225] Perez-Boada M, Ruiz-Duenas FJ, Pogni R, Basosi R, Choinowski T, Martinez MJ, et al. Versatile peroxidase oxidation of high redox potential aromatic compounds: site-directed mutagenesis, spectroscopic and crystallographic investigation of three long-range electron transfer pathways. *J Mol Biol* 2005;354:385–402.
- [226] Sáez-Jiménez V, Fernández-Fueyo E, Medrano FJ, Romero A, Martínez AT, Ruiz-Dueñas FJ. Improving the pH-stability of versatile peroxidase by comparative structural analysis with a naturally-stable manganese peroxidase. *PLoS One* 2015;10:e0140984.
- [227] Zeng J, Mills MJ, Simmons BA, Kent MS, Sale KL. Understanding factors controlling depolymerization and polymerization in catalytic degradation of β -ether linked model lignin compounds by versatile peroxidase. *Green Chem* 2017;19:2145–54.
- [228] Baratto MC, Juarez-Moreno K, Pogni R, Basosi R, Vazquez-Duhalt R. EPR and LC-MS studies on the mechanism of industrial dye decolorization by versatile peroxidase from *Bjerkandera adusta*. *Environ Sci Pollut Res Int* 2015;22:8683–92.
- [229] Kong W, Fu X, Wang L, Alhujaily A, Zhang J, Ma F, et al. A novel and efficient fungal delignification strategy based on versatile peroxidase for lignocellulose bioconversion. *Biotechnol Biofuels* 2017;10:218.
- [230] Salame TM, Knop D, Levinson D, Majeesh SJ, Yarden O, Hadar Y. Inactivation of a *Pleurotus ostreatus* versatile peroxidase-encoding gene (*mnp2*) results in reduced lignin degradation. *Environ Microbiol* 2014;16:265–77.
- [231] Mohorčić M, Benčina M, Friedrich J, Jerala R. Expression of soluble versatile peroxidase of *Bjerkandera adusta* in *Escherichia coli*. *Bioresour Technol* 2009;100:851–8.
- [232] Garcia-Ruiz E, Gonzalez-Perez D, Ruiz-Duenas FJ, Martinez AT, Alcalde M. Directed evolution of a temperature-, peroxide- and alkaline pH-tolerant versatile peroxidase. *Biochem J* 2012;441:487–98.
- [233] Pollegioni L, Tonin F, Rosini E. Lignin-degrading enzymes. *FEBS J* 2015;282:1190–213.
- [234] Kim SJ, Shoda M. Purification and characterization of a novel peroxidase from *Geotrichum candidum* dec 1 involved in decolorization of dyes. *Appl Environ Microbiol* 1999;65:1029–35.
- [235] de Gonzalo G, Colpa DI, Habib MH, Fraaije MW. Bacterial enzymes involved in lignin degradation. *J Biotechnol* 2016;236:110–9.
- [236] van Bloois E, Pazmiño DET, Winter RT, Fraaije MW. A robust and extracellular heme-containing peroxidase from *Thermobifida fusca* as prototype of a bacterial peroxidase superfamily. *Appl Microbiol Biotechnol* 2010;86:1419–30.
- [237] Liers C, Aranda E, Strittmatter E, Piontek K, Plattner DA, Zorn H, et al. Phenol oxidation by DyP-type peroxidases in comparison to fungal and plant peroxidases. *J Mol Catal B Enzym* 2014;103:41–6.
- [238] Sugano Y, Muramatsu R, Ichiiyanagi A, Sato T, Shoda M. DyP, a unique dye-decolorizing peroxidase, represents a novel heme peroxidase family: ASP171 replaces the distal histidine of classical peroxidases. *J Biol Chem* 2007;282:36652–8.
- [239] Brown ME, Barros T, Chang MC. Identification and characterization of a multifunctional dye peroxidase from a lignin-reactive bacterium. *ACS Chem Biol* 2012;7:2074–81.
- [240] Fawal N, Li Q, Savelli B, Brette M, Passaia G, Fabre M, et al. PeroxiBase: a database for large-scale evolutionary analysis of peroxidases. *Nucleic Acids Res* 2012;41:D441–4.
- [241] Abdel-Hamid AM, Solbiati JO, Cann IK. Insights into lignin degradation and its potential industrial applications. *Adv Appl Microbiol* 2013;1–28.
- [242] Brown ME, Chang MC. Exploring bacterial lignin degradation. *Curr Opin Chem Biol* 2014;19:1–7.
- [243] Singh R, Grigg JC, Qin W, Kadla JF, Murphy ME, Eltis LD. Improved manganese-oxidizing activity of DypB, a peroxidase from a lignolytic bacterium. *ACS Chem Biol* 2013;8:700–6.
- [244] Rahmanpour R, Rea D, Jamshidi S, Fulop V, Bugg TD. Structure of *Thermobifida fusca* DyP-type peroxidase and activity towards Kraft lignin and lignin model

- compounds. *Arch Biochem Biophys* 2016;594:54–60.
- [245] Avram A, Sengupta A, Pfromm PH, Zorn H, Lorenz P, Schwarz T, et al. Novel DyP from the basidiomycete *Pleurotus sapidus*: substrate screening and kinetics. *Biocatalysis* 2018;4:1–13.
- [246] Brissos Vn, Tavares D, Sousa AC, Robalo MP, Martins LO. Engineering a bacterial DyP-type peroxidase for enhanced oxidation of lignin-related phenolics at alkaline pH. *ACS Catal* 2017;7:3454–65.
- [247] Reiter J, Strittmatter H, Wiemann LO, Schieder D, Sieber V. Enzymatic cleavage of lignin β -O-4 aryl ether bonds via net internal hydrogen transfer. *Green Chem* 2013;15:1373–81.
- [248] Sato Y, Moriuchi H, Hishiyama S, Otsuka Y, Oshima K, Kasai D, et al. Identification of three alcohol dehydrogenase genes involved in the stereospecific catabolism of arylglycerol- β -aryl ether by *Sphingobium* sp. strain SYK-6. *Appl Environ Microbiol* 2009;75:5195–201.
- [249] Gall DL, Ralph J, Donohue TJ, Noguera DR. A group of sequence-related sphingomonad enzymes catalyzes cleavage of β -aryl ether linkages in lignin β -guaiacyl and β -syringyl ether dimers. *Environ Sci Technol* 2014;48:12454–63.
- [250] Picart P, Müller C, Mottweiler J, Wiermans L, Bolm C, Domínguez de María P, et al. From gene towards selective biomass valorization: bacterial β -etherases with catalytic activity on lignin-like polymers. *ChemSusChem* 2014;7:3164–71.
- [251] Masai E, Katayama Y, Fukuda M. Genetic and biochemical investigations on bacterial catabolic pathways for lignin-derived aromatic compounds. *Biosci Biotechnol Biochem* 2007;71:1–15.
- [252] Mnich E, Vanholme R, Oyarce P, Liu S, Lu F, Goeminne G, et al. Degradation of lignin β -aryl ether units in *Arabidopsis thaliana* expressing LigD, LigF and LigG from *Sphingomonas paucimobilis* SYK-6. *Plant Biotechnol J* 2017;15:581–93.
- [253] Sonoki T, Obi T, Kubota S, Higashi M, Masai E, Katayama Y. Coexistence of two different O demethylation systems in lignin metabolism by *Sphingomonas paucimobilis* SYK-6: cloning and sequencing of the lignin biphenyl-specific O-demethylase (LigX) gene. *Appl Environ Microbiol* 2000;66:2125–32.
- [254] Peng X, Egashira T, Hanashiro K, Masai E, Nishikawa S, Katayama Y, et al. Cloning of a *Sphingomonas paucimobilis* SYK-6 gene encoding a novel oxygenase that cleaves lignin-related biphenyl and characterization of the enzyme. *Appl Environ Microbiol* 1998;64:2520–7.
- [255] Pieper DH. Aerobic degradation of polychlorinated biphenyls. *Appl Microbiol Biotechnol* 2005;67:170–91.